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TECHNICAL REPORT

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$Li - SF_6$ COMBUSTION IN STORED CHEMICAL ENERGY PROPULSION SYSTEMS

S.H. Chan, C.C. Tan, Y.G. Zhao and P.J. Janke

Prepared for the Department of the Navy
Office of Naval Research
Arlington, VA 22217

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***Li - SF₆* COMBUSTION IN STORED CHEMICAL ENERGY PROPULSION SYSTEMS**

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TABLE OF CONTENTS

	Page
ABSTRACT.	1v
ACKNOWLEDGEMENT	v
LIST OF TABLES	vi
LIST OF FIGURES	vii
NOMENCLATURE.	x
1. INTRODUCTION.	1
2. EQUILIBRIUM STATE RELATIONSHIPS	2
2.1 Formulation.	2
2.2 Li-SF ₆ Reaction System	3
2.3 Thermodynamic Data	4
2.4 Comparison with Experimental Data.	5
2.5 Equilibrium Results.	5
3. STRUCTURE OF SF ₆ JETS IN MOLTEN Li	8
3.1 Mathematical Model	8
3.2 Comparison with Experimental Data.	9
3.3 Li-SF ₆ Flow Structure	9
3.4 Subcooling Effect.	11
3.5 Plume Length Correlation	12
4. CONCLUSIONS	13
REFERENCES.	14
APPENDIX A.	55
APPENDIX B.	141
ONR REPORT DISTRIBUTION LIST.	217

ABSTRACT

Appropriate thermodynamic models and thermo-chemical data for multicomponents and immiscible phases have been incorporated into a code for the computation of chemical equilibrium of the reactants used in a stored chemical energy propulsion system. The reactants considered are molten lithium fuel and gaseous sulfur hexafluoride oxidant. Extensive equilibrium state relationships as a function of mixture fraction have been presented over a temperature range of possible operating conditions. They were subsequently employed to predict the complex flow structure of a choked, turbulent, reacting SF_6 gas jet submerged in a molten lithium bath. Detailed profiles of velocity, temperature, void fraction and mass fraction of all phases in the jet have been presented. The results show that the reaction is completed within a short distance from the injector but the plume jet penetrates farther beyond due to significant evaporation of lithium fuel in the hot temperature plume, and subsequent condensation of the evaporated fuel and reaction products in the later part of the plume. The effect of lithium subcooling on flow structure has also been examined. It is found that lowering the degree of subcooling by raising the fuel bath temperature increases fuel evaporation, decreases the entrainment rate, delays the completion of reaction and lengthens greatly the jet penetration distance. Finally, for practical use, a simple correlation of the jet penetration length as a function of subcooling has also been presented.

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<i>A-1</i>	

LIST OF TABLES

<u>Table</u>	<u>Title</u>	<u>Page</u>
Table 1.	Subcooling Effects on Plume Length.	16

LIST OF FIGURES

<u>Figure</u>	<u>Title</u>	<u>Page</u>
Fig. 1.	Solubility Comparison Between Prediction (dots) and Data of Li-Li ₂ S System.	17
Fig. 2.	Equilibrium States (of Molten Li fuel at T _∞ = 1130 K reacting with gaseous SF ₆ at T ₀ = 298 K) Phase Diagram	18
Fig. 3.	Equations of States For Li - SF ₆ System with Li at 1130 K and SF ₆ Gas at 298 K.	19
Fig. 4.	Equations of States for Li - SF ₆ System with Li at 1358 K and SF ₆ Gas at 298 K.	20
Fig. 5.	Equations of States for Li - SF ₆ System with Li at 1415 K and SF ₆ Gas at 298 K.	21
Fig. 6.	Equations of States for Li - SF ₆ System with Li at 1586 K and SF ₆ Gas at 298 K.	22
Fig. 7	Equilibrium Compositions of Li - SF ₆ System with Li at 1130 K and SF ₆ Gas at 298 K.	23
Fig. 8	Equilibrium Compositions of Li - SF ₆ System with Li at 1358 K and SF ₆ Gas at 298 K.	24
Fig. 9	Equilibrium Compositions of Li - SF ₆ System with Li at 1415 K and SF ₆ Gas at 298 K.	25
Fig. 10	Equilibrium Compositions of Li - SF ₆ System with Li at 1586 K and SF ₆ Gas at 298 K.	26
Fig. 11	Equilibrium Compositions of Li - SF ₆ System with Li at 1130 K and SF ₆ Gas at 298 K.	27
Fig. 12	Equilibrium Compositions of Li - SF ₆ System with Li at 1358 K and SF ₆ Gas at 298 K.	28
Fig. 13	Equilibrium Compositions of Li - SF ₆ System with Li at 1415 K and SF ₆ Gas at 298 K.	29
Fig. 14	Equilibrium Compositions of Li - SF ₆ System with Li at 1586 K and SF ₆ Gas at 298 K.	30
Fig. 15	Equilibrium Compositions of Li - SF ₆ System with Li at 1130 K and SF ₆ Gas at 298 K.	31
Fig. 16	Equilibrium Compositions of Li - SF ₆ System with Li at 1358 K and SF ₆ Gas at 298 K.	32
Fig. 17	Equilibrium Compositions of Li - SF ₆ System with Li at 1415 K and SF ₆ Gas at 298 K.	33

Fig. 18	Equilibrium Compositions of Li - SF ₆ System with Li at 1586 K and SF ₆ Gas at 298 K.	34
Fig. 19	Equilibrium Compositions of Li - SF ₆ System with Li at 1130 K and SF ₆ Gas at 298 K.	35
Fig. 20	Equilibrium Compositions of Li - SF ₆ System with Li at 1358 K and SF ₆ Gas at 298 K.	36
Fig. 21	Equilibrium Compositions of Li - SF ₆ System with Li at 1415 K and SF ₆ Gas at 298 K.	37
Fig. 22	Equilibrium Compositions of Li - SF ₆ System with Li at 1586 K and SF ₆ Gas at 298 K.	38
Fig. 23	Equilibrium Compositions of Li - SF ₆ System with Li at 1130 K and SF ₆ Gas at 298 K.	39
Fig. 24	Equilibrium Compositions of Li - SF ₆ System with Li at 1358 K and SF ₆ Gas at 298 K.	40
Fig. 25	Equilibrium Compositions of Li - SF ₆ System with Li at 1415 K and SF ₆ Gas at 298 K.	41
Fig. 26	Equilibrium Compositions of Li - SF ₆ System with Li at 1586 K and SF ₆ Gas at 298 K.	42
Fig. 27	Equilibrium Compositions of Li - SF ₆ System with Li at 1130 K and SF ₆ Gas at 298 K.	43
Fig. 28	Equilibrium Compositions of Li - SF ₆ System with Li at 1358 K and SF ₆ Gas at 298 K.	44
Fig. 29	Equilibrium Compositions of Li - SF ₆ System with Li at 1415 K and SF ₆ Gas at 298 K.	45
Fig. 30	Equilibrium Compositions of Li - SF ₆ System with Li at 1586 K and SF ₆ Gas at 298 K.	46
Fig. 31	Equilibrium Compositions of Li - SF ₆ System with Li at 1130 K and SF ₆ Gas at 298 K.	47
Fig. 32	Equilibrium Compositions of Li - SF ₆ System with Li at 1358 K and SF ₆ Gas at 298 K.	48
Fig. 33	Equilibrium Compositions of Li - SF ₆ System with Li at 1415 K and SF ₆ Gas at 298 K.	49
Fig. 34	Equilibrium Compositions of Li - SF ₆ System with Li at 1586 K and SF ₆ Gas at 298 K.	50
Fig. 35	Predicted Mean Quantities Along the Jet Axis SF ₆ Gas at (298 K) Discharged in Molten Li (1130 K).	51

Fig. 36	Predicted Mean Quantities Along the Jet Axis SF_6 Gas at (298 K) Discharged in Molten Li (1358 K).	52
Fig. 37	Predicted Mean Quantities Along the Jet Axis SF_6 Gas at (298 K) Discharged in Molten Li (1415 K).	53
Fig. 38	Predicted Mean Quantities Along the Jet Axis SF_6 Gas at (298 K) Discharged in Molten Li (1586 K).	54

NOMENCLATURE

A_{ij}	interpreted as interaction energy
b_i	quasi-lattice parameters
C_p	specific heat
D	injector diameter
f	mixture fraction
g	the square of mixture fraction fluctuation
ΔH_r	heat of reaction
K	turbulent kinetic energy
L	plume length
N_i	moles of chemical species i
R	gas constant
T	Temperature
u	axial velocity
x	axial distance
Y	mass fraction

Greek Symbols

γ_k	activity coefficient of k th species
ρ	density
ϵ	turbulent dissipation rate

Superscripts

\sim	Favre averaged quantities
$-$	time averaged quantities

Subscripts

k	k species
0	jet nozzle condition
∞	bath (or surrounding) condition
S	solid
L	liquid
G	gas
d	down stream
u	up stream

1. INTRODUCTION

After an extended period of study,¹⁻⁵ the closed Rankine-cycle, lithium fueled SCEPS (Stored Chemical Energy Propulsion System) has emerged as the best choice for undersea propulsion system.⁶⁻⁷ The SCEPS derives its chemical heat source from the highly exothermic reaction between an alkali liquid metal fuel and a halogen gas oxidant. The reactants are so selected to yield several advantages and unique features for underwater propulsion. First, the energy density value is exceptionally high on a total reactants (fuel plus oxidant) gravimetric basis. Secondly, the products of combustion are in condensed (liquid and solid) phases and their combined density is greater than the density of molten fuel. These characteristics permit the use of a closed reactor for a near-constant volume, bath-type combustion process. Furthermore, the reactor initially holding the molten metal fuel will become the holding tank to house combustion products and no discharge of products from the reactor to the environment is necessary. Coupling this thermal energy source reactor to a closed Rankine steam cycle to propel a turbine, the performance of such a combined power system is therefore insensitive to operating depth, making it well suited for undersea applications.

Among reactants for undersea propulsion, the use of lithium (Li) fuel with sulfur hexafluoride (SF_6) oxidant appears to be the best candidate for the SCEPS concept. They are relatively economical. The SF_6 oxidant is inert and non-toxic. The heat of reaction based on a unit mass of total reactants exceeds even that of H_2/O_2 reactants.¹ They are being adopted for the on-going SCEPS project. However, to the authors' best knowledge, the flow structure analysis of turbulent SF_6 gas jets submerged in and reacting with a molten lithium has not been reported in the literature.

Prior work on the related subject is very limited. A Na/Cl system was analyzed by a simplified integral model⁸ which was improved⁹ by the use of the local homogeneous flow approximation, equilibrium combustion model and κ - ϵ -g model.¹⁰ The predictions seem to agree with the data of a highly diluted, non-evaporating sodium fuel.⁸ Later it was incorporated into the model a general scheme for complex equilibrium computation for nonideal multi-phase electrolytic system,¹¹ which was tested successfully with the data¹² of a reacting, evaporating and condensing system--HCl/aqueous ammonia solution containing up to 25% of $\text{NH}_3(\text{aq})$ to simulate the metal fuel.

This study draws from the prior works^{9,11} and extends to Li/SF₆ system. Specifically, the thermodynamic properties of the multiphase, nonideal reacting mixture of Li_(L)/SF_{6(g)} reactants in chemical equilibrium are constructed and presented as a function of mixture fraction (state relationships). They are then used to predict the turbulent flame structure of Li/SF₆ reacting jets. The former provides the fundamental information useful for combustion studies in general while the latter predicts the detailed flow structure of the complex flame-like jets which may contain several liquid and solid phases due to partial miscibility of molten lithium fuel and its reaction salt product, lithium fluoride.

2. EQUILIBRIUM STATE RELATIONSHIPS

2.1 Formulation

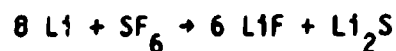
The information on equilibrium state relationships are prerequisite to the analysis of the flame structure of a SF₆ gas jet reacting in a molten Li fuel. The required relationships include equilibrium compositions of all species in all phases, the equilibrium temperature and density of the mixture resulting from the reaction of molten Li with gaseous SF₆ at various mixture fractions.

The general formulation for the state relationships has been described earlier.^{9,11} Briefly, it utilizes a variation of the direct Gibbs free energy minimization approach. The minimization is subject to element abundance and charge balance constraints. A general purpose code was developed for complex equilibrium computation for nonideal multiphase systems (CEC-NMS), which has been extensively tested^{11,13} for a simulant reactant pair of HCl as oxidant and aqueous ammonia solution as fuel to confirm the validity of the overall approach.

One of the objectives in the present study is to include in the code the specific thermodynamic models and the necessary thermo-chemical property data of the SF_6 -Li reacting system and then perform the complex equilibrium computation of the SF_6 and Li reactants for SCEPS.

2.2 Li-SF₆ Reaction System

The stoichiometric reaction between lithium and sulfur hexafluoride can be expressed as³



which liberates a large amount of thermal energy and produces lithium fluoride, the dominant product, and lithium sulfide, the minor product. For generality, whether the reaction is stoichiometric or not, the gas phase of the reacting mixture in the present study allows for the possible existence of fifteen species. They are Li, Li₂, F, F₂, LiF, Li₂F₂, Li₃F₃, SF, SF₂, SF₄, SF₆, S₂F₂, Li₂S, S and S₂, which are assumed to behave as an ideal gas mixture. Four solid species are considered in separate phases: Li_(s), LiF_(s), S_(s) and Li₂S_(s).

The liquid phase is assumed to contain three possible species: Li_(L), LiF_(L) and Li₂S_(L). The liquid metal, Li_(L), and the molten salt, LiF_(L), can form two immiscible phases with an additional component, Li₂S_(L), dissolved

in each phase to form ternary mixtures. The activity coefficients of the immiscible liquid phases (metal-rich phase (L-1) and salt-rich phase (L-2)) are predicted using the multicomponent van Laar model.¹⁴ The activity coefficient of the kth species may be given as

$$\ln \gamma_k = b_k \sum_i \sum_j (A'_{ik} - 0.5A'_{ij}) b_i b_j N_i N_j / [RT (\sum_i N_i b_i)^2] \quad (1)$$

where A'_{ij} and b_i are empirical parameters. Note that $A'_{ii} = 0$, and $A'_{ij} = A'_{ji}$. The equation given here differs from that presented by Groff and Faeth (ref. 15, p. 22, and ref. 16, p. 328). We believe this equation to be the correct one.

For a system with three components, the number of empirical parameters may be reduced by one by defining new parameters A_{ij} and B_i as¹⁵:

$$A_{ij} = b_i A'_{ij}; \quad B_1 = b_1/b_2; \quad B_2 = b_2/b_3; \quad \text{and} \quad B_3 = b_1/b_3 = B_1 B_2 \quad (2)$$

The subscripts 1, 2, and 3 refer to $\text{Li}_{(L)}$, $\text{LiF}_{(L)}$, and $\text{Li}_2\text{S}_{(L)}$, respectively. Equation (1) may then be written as

$$\ln \gamma_k = \sum_i \sum_j (A_{ik} - 0.5A_{ij}) (b_j/b_k) N_i N_j / RT [\sum_i N_i (b_i/b_k)]^2 \quad (3)$$

The estimated empirical parameters, A_{ij} , from experimental data in units of (kJ/mole) are a function of temperature (K) as,¹⁵

$$A_{12} = 121.53 - 0.05730 T; \quad A_{13} = 53.287 - 4.00E-4 T; \quad A_{23} = 0 \quad (4)$$

$$B_1 = 2.5846 - 8.132E-4 T; \quad B_3 = 1.36; \quad B_2 = B_3/B_1 \quad (5)$$

2.3 Thermodynamic Data

Thermodynamic data for all three forms of Li_2S is extremely limited. Groff and Faeth¹⁵ estimated the required spectroscopic data for determining

the properties of $\text{Li}_2\text{S}_{(g)}$ using statistical methods. They felt the accuracy of the resulting thermodynamic data for $\text{Li}_2\text{S}_{(g)}$ to be within $\pm 5\%$. Their equations are used in this work to calculate the enthalpy and Gibbs energy of gaseous lithium sulfide. They also estimated thermodynamic data for $\text{Li}_2\text{S}_{(s)}$ and $\text{Li}_2\text{S}_{(l)}$ from Na_2S , Li_2O , and Na_2O using Kopp's rule.¹⁷ Their estimated values were used to calculate the enthalpy and Gibbs energy for solid and liquid lithium sulfide. The thermodynamic data for all other species were taken from the data file provided with the CEC-72 computer program.¹⁸

2.4 Comparison with Experimental Data

The equilibrium results to be presented later involve a multiphase and multi-species system. No experimental data is available to compare these results to, nor have any calculations of this type appeared in the literature. It is decided to test the validity of the above thermodynamic model and the accuracy of the numerical calculations by computing the phase equilibrium diagrams of binary systems of which experimental data are available for comparison. The tests include $\text{Li-Li}_2\text{S}$, Li-LiF , and $\text{LiF-Li}_2\text{S}$ binary systems. A representative comparison between the prediction (indicated by dots) and experimental data^{16,19} (line) of the $\text{Li-Li}_2\text{S}$ binary is shown in Fig. 1. Good agreement was found in all binaries.

2.5 Equilibrium Results

The above thermodynamic model and data have been properly incorporated into CEC-NMS code to calculate equilibrium state relationships. As stated above, the resulting code has been tested against the binary data and is now ready for multi-species computations. The equilibrium results are presented in Figs. 3 to 6 for the reaction of a gaseous SF_6 at $T_0 = 298 \text{ K}$ with a

molten Li at $T_{\infty} = 1130$ K, 1358 K, 1415 K, 1586 K, respectively and one atmosphere pressure.

Figure 3 to 6 show the equilibrium temperature, density, void fraction, mass fractions of gas, liquid and solid phases as a function of mixture fraction f . The latter is so defined that $f = 1$ designates the pure SF_6 gas and $f = 0$ indicates the pure molten Li metal. In Figs. 7 to 34 the corresponding mass fractions of all individual species in each of three phases are provided. By referring to Figs. 3 to 6, as the value of f in the reacting system decreases from one, the equilibrium temperature increases while the mixture density decreases. However, the temperature is still low enough that a condensed solid phase of $\text{LiF}_{(s)}$ emerges in a narrow range and another condensed liquid phase of $\text{LiF}_{(L)}$ also appears in a narrow range, which can be verified by checking Figs. 11 to 14. The co-existed gas phase is composed of the excess SF_6 gas and vapors of combustion products. As f decreases to the stoichiometric value of $f_{st} = 0.72$, where temperature reaches the maximum and density the minimum, all species are turned into gaseous/vapor phase. Further decreasing in f will result in a lower temperature, higher density and the appearance of a liquid phase. Since molten Li and LiF liquids are partially immiscible, which is accounted for in the present formulation, one might expect co-existence of two liquids: metal rich phase (L-1) and salt-rich phase (L-2). However our equilibrium results reveal only one liquid in existence at a time. This can be explained as follows.

The necessary condition for two liquids to co-exist is that the mixture is fuel-rich, i.e., when $0 < f < f_{st}$. However in most of region in $f = 0$ to f_{st} , the mixture equilibrium temperature exceeds the consolute temperature (1600 K), the maximum temperature above which two immiscible liquids can not co-exist. Naturally, only single liquid exists. For the rest of the region,

LiF is below the solubility limit so that again only one liquid exists. A clear picture can be seen by referring to the Li-LiF phase diagram^{16,19} shown in Fig. 2. The equilibrium states in the present study all lie in the one liquid region above the two-liquid dome. For this reason, the computer printouts do not discern (L-1) liquid from (L-2) liquid and similar species are lumped together. For example, in Figs. 23 to 26, the liquid lithium fuel species is then indicated by $(Li_{(L-1)} + Li_{(L-2)})$ or $(Li_{(L-1)})$, and so forth.

From the results of the current equilibrium state relationships, one can expect that no two immiscible liquids will co-exist in the reacting plume to be studied in the later section. However, it does not preclude the two immiscible liquids from forming outside the plume region when the mixture temperature drops because of heat losses to surrounding heat exchangers.

It is interesting to point out that for the identical initial oxidant temperature of 298 K and the fuel temperature of 1130 K, an immiscible liquid region does appear in sodium-chlorine reacting system,⁹ but not in the present lithium-sulfur hexafluoride system. Had the initial bath temperature of lithium been lower, it is likely that the solubility limit of the salt in the metal would have been reached at a lower temperature. Then the salt-rich liquid would begin to form at a temperature below the consolute temperature and an immiscible liquid region would appear.

Similar equilibrium results have been obtained for lithium fuel maintained at four elevated temperatures listed in Table 1. They will be used later in the study of subcooling effects on the flow structure of SF_6 jets reacting in molten Li pools.

3. STRUCTURE OF SF_6 JETS IN MOLTEN LI

3.1 Mathematical Model

The combustor under consideration is a large vessel filled with a molten Li fuel at one atmospheric pressure. A gaseous oxidant SF_6 drawn from a liquefied storage tank, is discharged into a large vessel through a small injector mounted at the bottom of the vessel. The choked, turbulent SF_6 gas jet will react with the entrained molten Li to form a complex, multiphase, axisymmetric jet. A steady jet is the subject under investigation. In practice, the fuel vessel is finite in size and the reaction is transient in nature. The current steady state calculation provides results at a given time. With the state relationships developed above, the structure of the steady reacting jet is to be predicted. The flow model adopted here follows closely the method developed previously.^{9,10} Basically, it employs the local homogeneous two-phase flow model, the local chemically equilibrium combustion model with the foregoing equilibrium state relations, and Shvab-Zeldovich type of formulation. The conserved equations to be solved are summarized in the previous papers^{9,11} and will not be re-iterated here. They include the Favre-averaged parabolic form of transport equations for continuity, momentum, mixture fraction (\tilde{f}), turbulence kinetic energy (k), the rate of turbulence dissipation (ϵ) and the square of the mixture fraction fluctuation (g). The mean scalar properties other than those from the solution of transport equations are determined locally in the plume by integrating the product of the corresponding equilibrium state relationships and a clipped Gaussian probability density profile over the entire range of the mixture fraction.

3.2 Comparison with Experimental Data

Again as in the state relationships, no experimental data nor numerical calculations are available for comparison with the flow structures of Li-SF₆ system to be presented next. However, the above mathematical model and the resulting modified GENMIX code developed in this laboratory were extensively tested using experimental data¹² of metal simulant reactants (HCl-NH₃ aqueous solution) in our recent studies^{11,13}. Good agreement was found between predictions and data for various fuel temperature, pressure and concentration conditions. The primary purpose of those studies is in fact to lay a ground work for the present liquid metal combustion study, the results of which are given below.

3.3 Li-SF₆ Flow Structure

The initial condition of the sulfur hexafluoride gas jet at the injector exit is assumed to be uniform and taken as^{11,13}

$$\begin{aligned} \rho_0 &= 5.97 \text{ Kg/m}^3, & T_0 &= 298 \text{ K}, & \tilde{u}_0 &= 203.4 \text{ m/s} \\ \tilde{f}_0 &= 1, & k_0 &= (0.03 \tilde{u}_0)^2, & \epsilon_0 &= (0.03 \tilde{u}_0)^3/D, & g_0 &= 0 \end{aligned} \quad (6)$$

The injector diameter $D = 7.9 \times 10^{-4} \text{ m}$ is used in the computation. At the plume center axis, the radial gradients of \tilde{u} , \tilde{f} , k , ϵ , and g are set to zero due to symmetry. At the outer boundary of the jet, $g = 0$, $\tilde{u} = 0.0005 u_0$ and $\tilde{f} = 0.0005 \tilde{f}_0$ are assumed, while k and ϵ are described by $k = (0.03 \tilde{u}_0)^2$, and $\epsilon = (0.03 \tilde{u}_0)^3/D$ at the first axial step. At later steps on the outer boundary,

$$k_d = k_u - \epsilon_u \Delta x / \tilde{u}_u; \quad \epsilon_d = \epsilon_u - C_{\epsilon 2} \epsilon_u^2 \Delta x / (k_u \tilde{u}_u) \quad (7)$$

which are obtained by solving the governing equations with the radial convective and diffusive terms neglected. The subscripts d and u denote the downstream and upstream points, respectively. The numerical computational details are given in the previous study.¹¹

Using the above initial and boundary conditions, and incorporating the equilibrium state relationships in the modified GENMIX code, the structure of a reacting SF_6 gas jet submerged in a molten lithium bath has been computed. Figs. 35-38 shows the predicted mean quantities along the center axis of the jet when the bath temperature is maintained separately at $T_\infty = 1130 \text{ K}$ and etc.,

in which 1 atm. pressure is maintained. Centerline velocity (\tilde{u}/\tilde{u}_0), mixture fraction (\tilde{f}), temperature (\tilde{T}), gas mass fraction (\tilde{Y}_g), liquid mass fraction (\tilde{Y}_l), solid mass fraction (\tilde{Y}_s) and void fraction ($\tilde{\alpha}$) are plotted against the dimensionless distance (x/D) from the injector exit. It is seen that the mixture temperature rises sharply in a narrow range of (x/D). Combustion products appear in solid and liquid phases with some overlapping near the injector due to relatively low mixture temperature. Then they turn into vapor phase around the high temperature zone and finally into liquid phase far away from the injector. The complete condensation of reaction products is one of the unique and desirable features of the SCEPS, which results in a relatively short plume length of $L/D = 5.6$. The plume length here is arbitrarily taken as the length where the void fraction reduces to 0.01. It is the total length which includes the reaction, evaporation and condensation regions. The flow structure computation indicates that the reaction region ends at $x/D = 3.9$ where the injected SF_6 oxidant is consumed almost completely (the mean mass fraction of SF_6 and all its derivatives like dissociated elements etc. reduces, say, to 0.001 along the jet axis). As the mixture temperature increases in the reaction region the evaporation of the molten Li entrained

into the jet stream from the surrounding bath becomes increasingly important. The excess evaporated fuel and combustion products are eventually condensed downstream. This evaporation-condensation region partially overlaps with the reaction region; its length is rather substantial and cannot be ignored. Further checking of species presented in the evaporation-condensation region indicates that the lithium fuel vapor outweighs the reaction product vapor. This can be explained if reference is made to the equilibrium composition in Figs. 11 to 14. Analogous to the flow structure diagram, the corresponding reaction region in Figs. 11 to 14 is approximately extended from $f = 1$ to 0.67 at which the oxidant SF_6 gas and its derivative components are practically all consumed in the reaction. Similarly the evaporation-condensation region lies between $f = 0.79$ to 0.13. It is clearly seen that in some evaporation-condensation region the mass fraction of fuel ($Li + Li_2$) vapor, indeed far exceeds that of the vapor product ($LiF + Li_2F_2 + Li_3F_3$).

3.4 Subcooling Effect

To investigate effects of subcooling on turbulent structure of reacting jets, the bath fuel temperature is varied from 1130 K to 1586 K as shown in Table 1. It covers practically all the possible operation range of SCEPS. Since the working temperature of the reactor must be so chosen that the reaction products are in liquid state, the lowest possible operation temperature is limited by the melting point of the mixture of lithium fluoride and lithium sulfide, which is 1083 K. Similarly, the maximum temperature is bounded by the saturation (boiling) temperature of lithium fuel, which is 1609 K.

Flow structures of all subcooling cases listed in Table 1 have been computed. Figures 35 to 38 show the effect of subcooling on the plume penetration. When the bath temperature is increased from 1130 to 1586 K, the

ooling temperature (i.e. saturation temperature minus bath temperature) is reduced from 479 K to 23 K (minimum subcooling), and the plume penetration length is also increased in an order of magnitude. In fact the reduction in fuel subcooling delays considerably the appearance of solid and liquid phases. Also delayed is the temperature peak which implies that the primary reaction occurs at further downstream from the injector. The latter is attributed to the reduction in the fuel entrainment rate in spite of increasing fuel evaporation. Since Li vapor is lighter than the Li liquid in the bath and SF_6 gas in the main jet stream, the jet mixture density decreases near the boundary as more Li evaporates from the jet interphase boundary. Consequently the turbulent viscosity and the entrainment rate of the ambient fuel are reduced accordingly. Similar phenomenon has been observed in the simulant reactant pair of hydrogen chloride gas reacting with ammonia solution.¹¹

3.5 Plume Length Correlation

The total penetration length is one of the key parameters needed for the design of the liquid metal combustor. It is desirable if the plume lengths from the above complex computation can be correlated by a simple equation for practical use.

With the consideration of a simple entrainment expression and the energy balance between the reaction heat release and heating and vaporization of the entrained fuel, the plume length could be grossly estimated as¹²

$$\frac{L}{D} = c \frac{\Delta H_r}{c_p \Delta T} \left(\frac{\rho_0}{\rho_\infty} \right)^{1/2} \quad (8)$$

where c is a correlation constant, ΔH_r is the heat of reaction per unit mass of oxidant, c_p is the specific heat of the bath liquid and ΔT is the

degree of subcooling of the bath liquid. Table 1 lists most of the relevant parameters including the computed plume lengths under various subcooling conditions. The L in the above equation represents the length over which all the reaction heat is dissipated by the sensible heat of the entrained liquid from the bath. It is consistent with the notion that the plume mostly consists of fuel vapor produced by reaction heat release and that the plume length is determined by the distance required for the condensation of the fuel vapor. The equation is essentially identical to the correlation of Weimer et al.²⁰ for their data on penetration lengths of condensing vapor jets in liquids. The c value proposed by Weimer et al.²⁰ is 17.8 which was also used for Na-Cl₂ system.^{8,12} For HCl-NH₃ aqueous solution system, about half of that value was suggested.¹² In the present Li-SF₆ reacting system, we attempt to correlate the subcooling effect by equation (8). The value of the correlation constant is found to be 5.506 by the least square method. The absolute deviation in the plume length of the correlation from the computed length is between 1.8 to 57%.

4. CONCLUSIONS

The liquid metal combustion in stored chemical energy propulsion system has been analyzed. The necessary thermodynamic data have been presented and incorporated into a general purpose code to account for nonideal solutions forming immiscible phases. Specifically, equilibrium state relationships of the gaseous SF₆-molten Li reacting system have been presented as a function of mixture fraction. Comparisons have been made with limited experimental data available and good agreement is found. Using the state relationships and appropriate flow models, the structure of sonic, turbulent, reacting SF₆ gas jets submerged in molten Li baths has been obtained. Velocity, temperature,

void fraction, and mass fractions of gas, liquid and solid phases, etc. in the reacting jets have been presented. The plume length is found to be finite, due to condensation of reaction products, but penetrates far beyond the reaction length because the lithium fuel evaporated in the high temperature region must be re-condensed in lower temperature region. The subcooling effect has also been examined and found to greatly affect the flow structure by shifting the structure downstream when the degree of subcooling is reduced. Finally a simple equation is presented which correlates the plume length as a function of subcooling satisfactorily. The results of the present study make possible the prediction of flow structure in the current design of SCEPS for undersea propulsion systems.

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Table 1. Subcooling effects on plume length

T_{∞}	Subcooling	ρ_{∞}	ρ_0	C_p	ΔH_r	$\frac{L}{d}$
K	$\Delta T, K$	Kg/m^3	Kg/m^3	$\frac{KJ}{Kg \text{ of } Li}$	$\frac{KJ}{Kg \text{ of } SF_6}$	
1130	479	449	5.97	4.13	19,267	5.66
1358	251	426	5.97	4.11	19,116	11.64
1415	194	421	5.97	4.10	19,079	36.44
1586	23	403	5.97	4.10	18,966	132.42

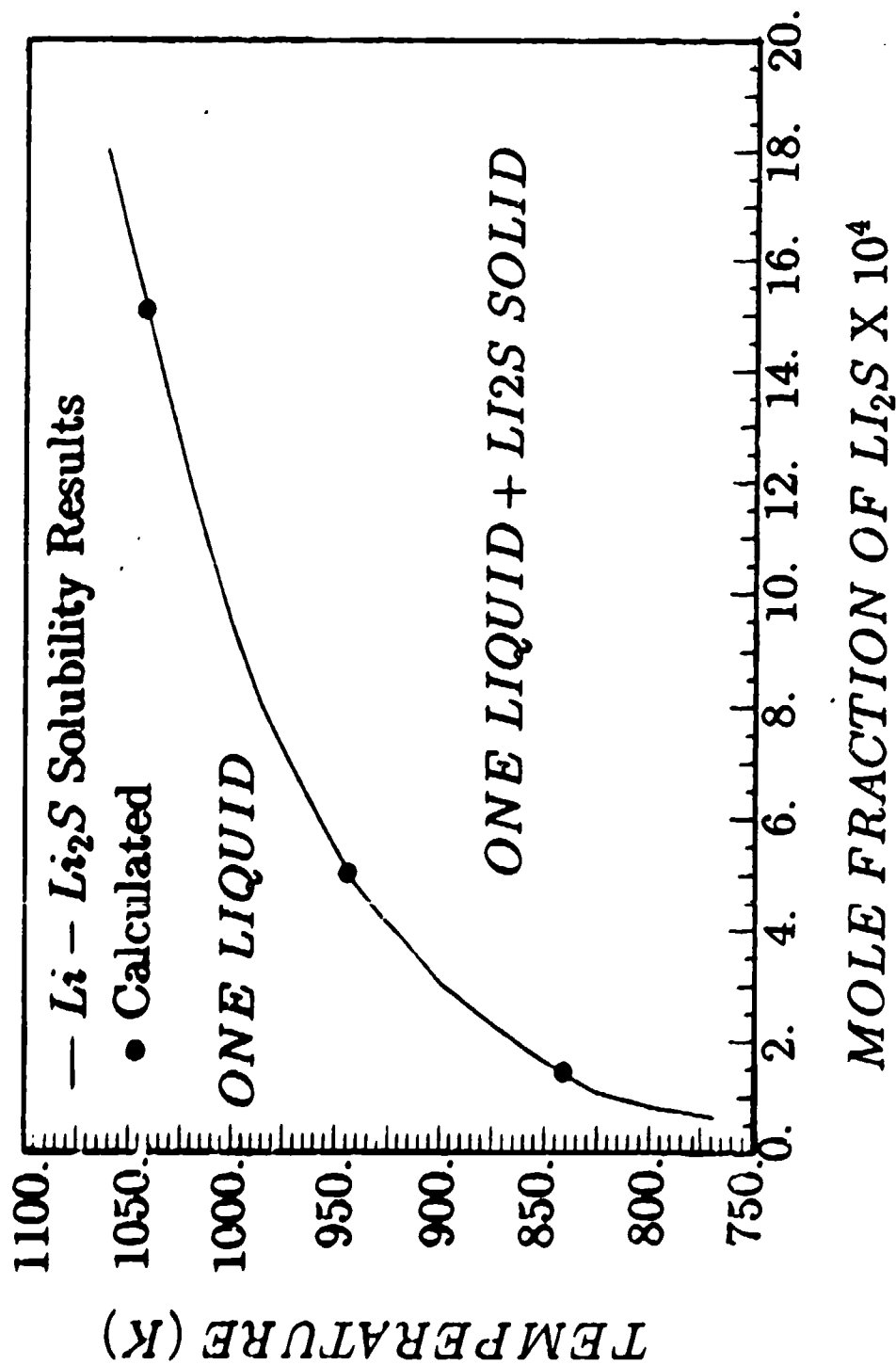


Fig.1 Solubility Comparison Between Prediction(dots) and Data of *Li - Li₂S* System

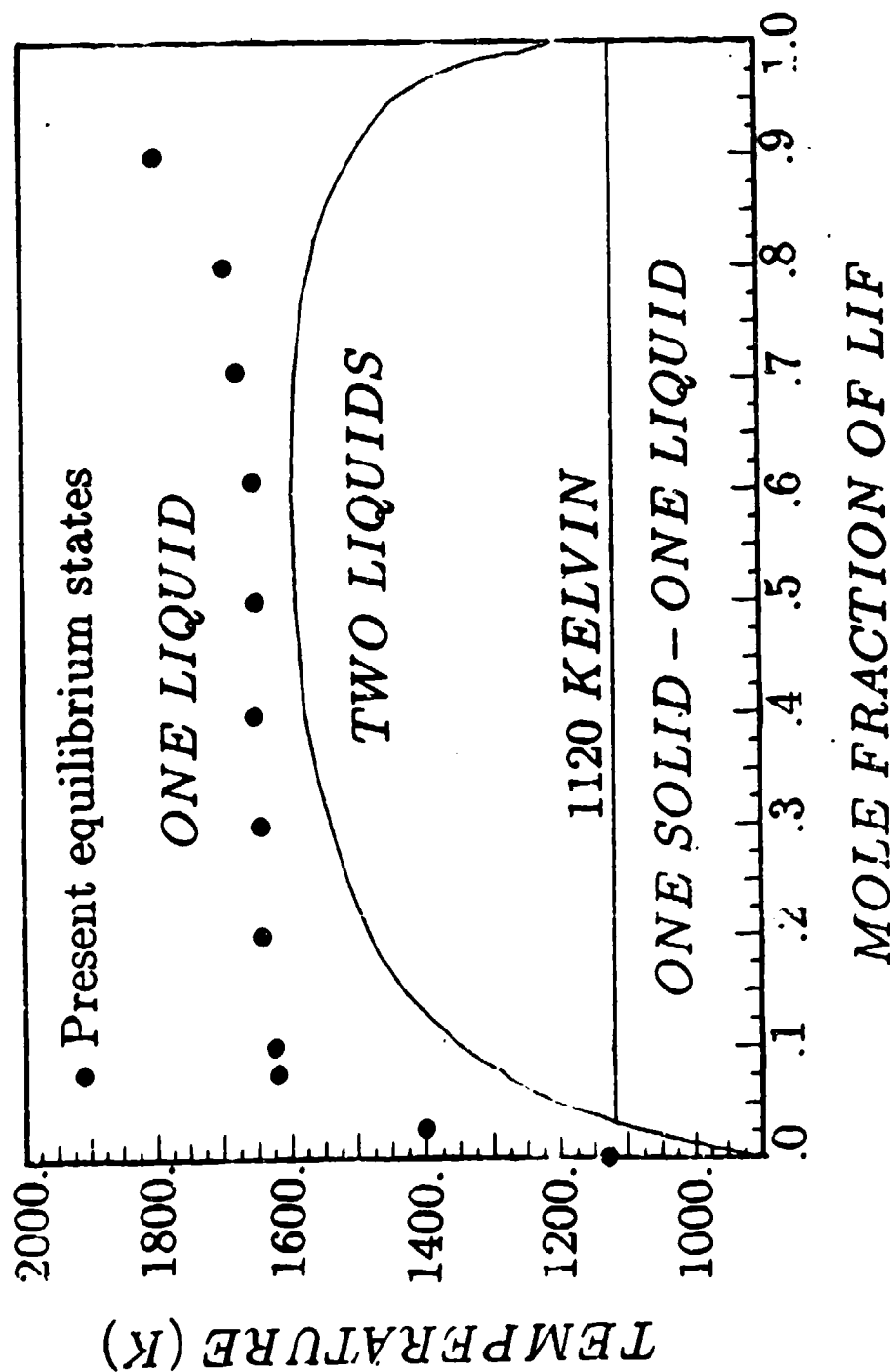


Fig.2 Equilibrium States (of Molten Li fuel at $T_{\infty}=1130$ K reacting with gaseous SF_6 at $T_0=298$ K) Phase Diagram

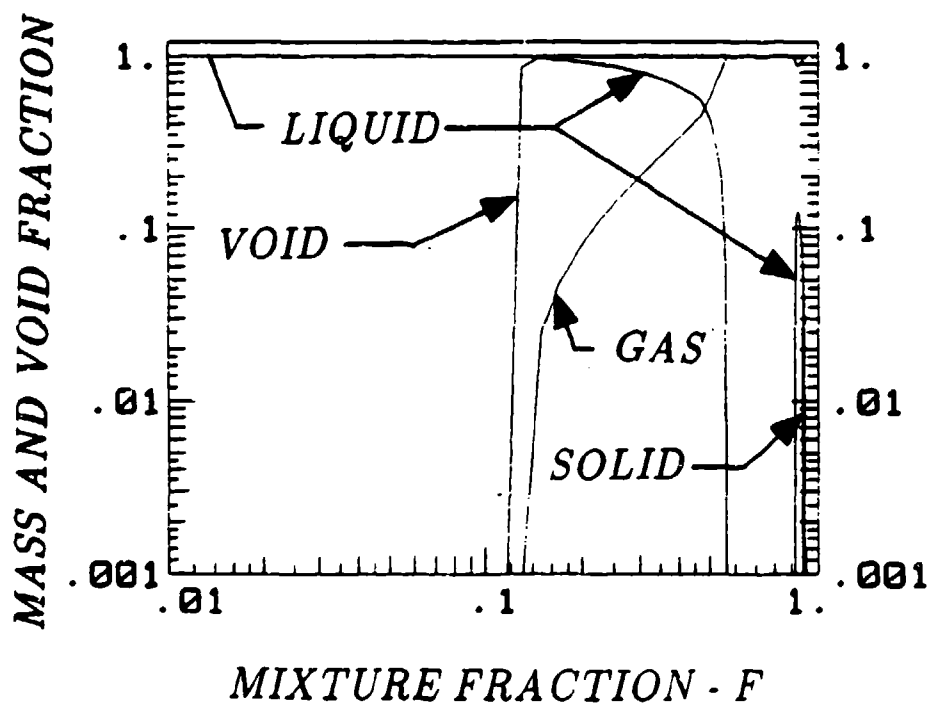
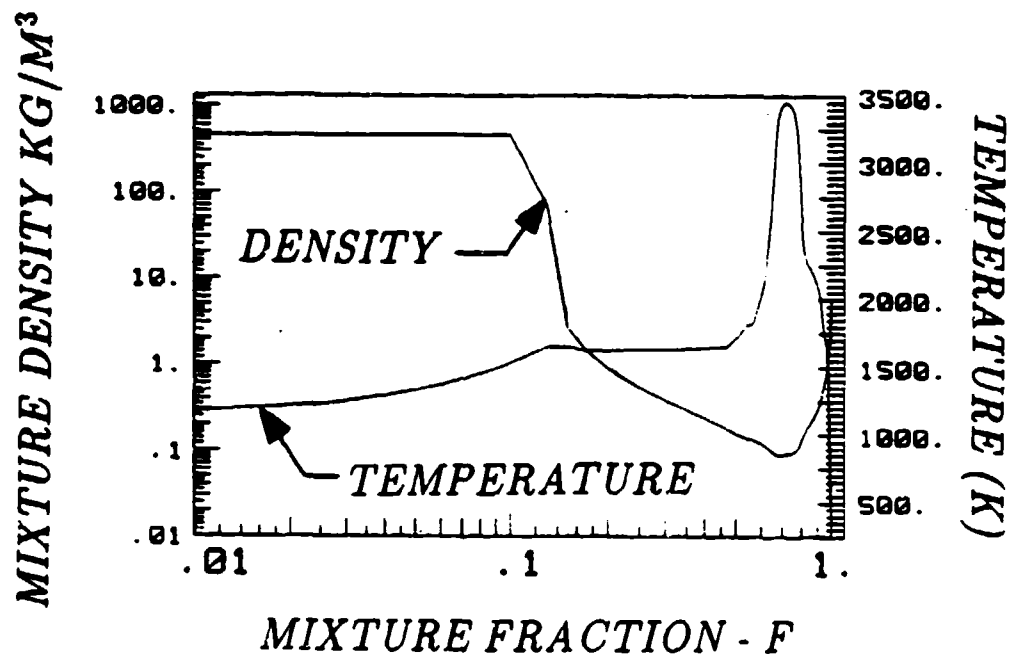


Fig.3 Equations of States For $\text{Li} - \text{SF}_6$ System with Li at 1130 K and SF_6 Gas at 298 K

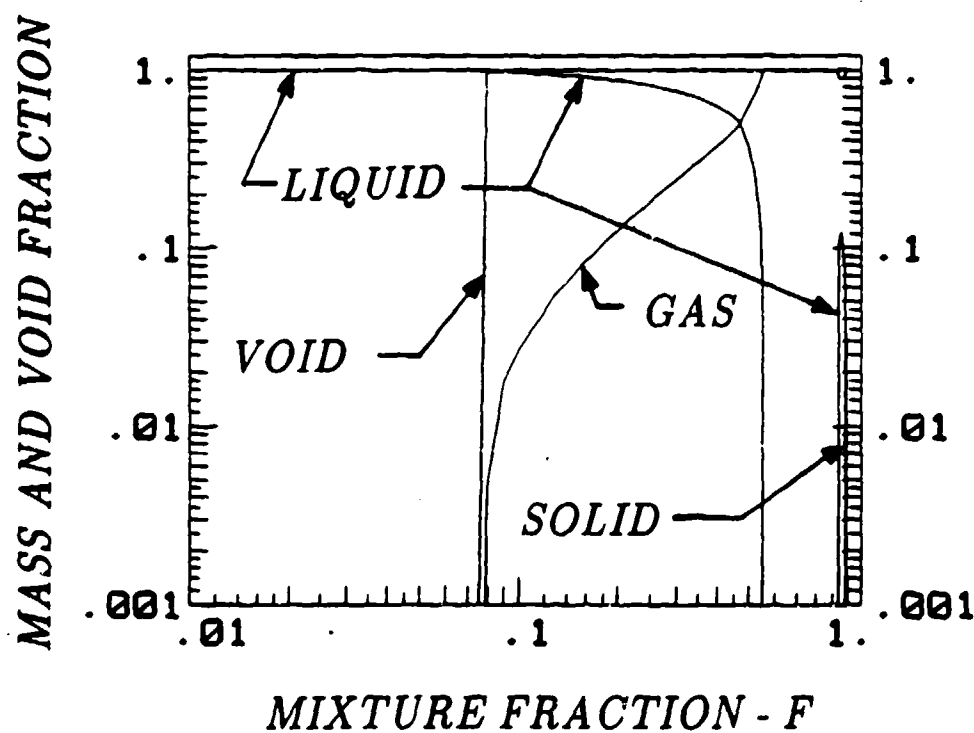
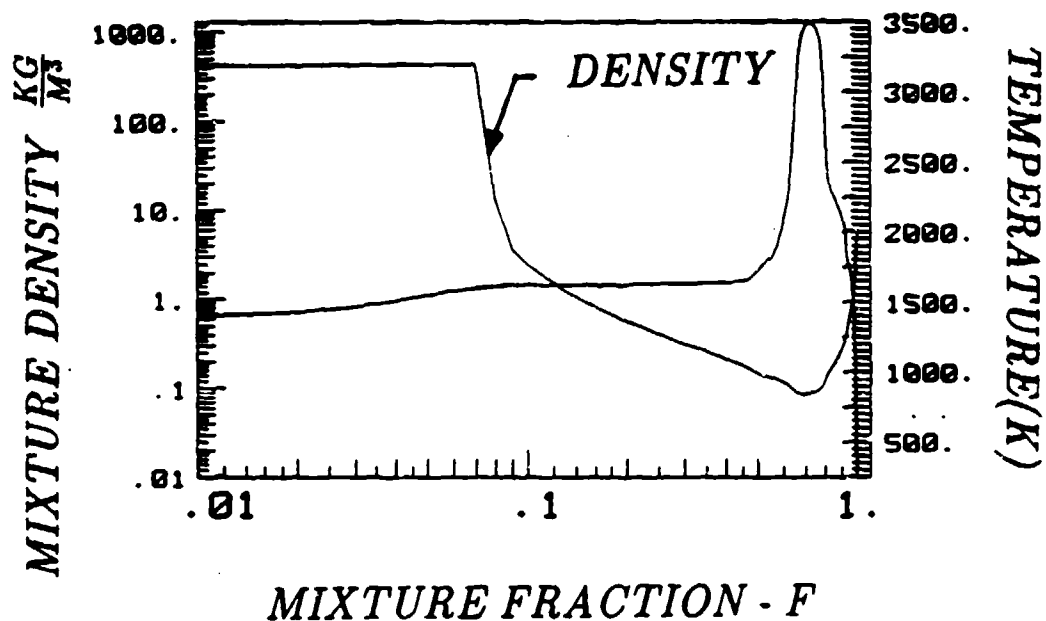


Fig.4 Equations of States For $\text{Li} - \text{SF}_6$ System with Li at 1358 K and SF_6 Gas at 298 K

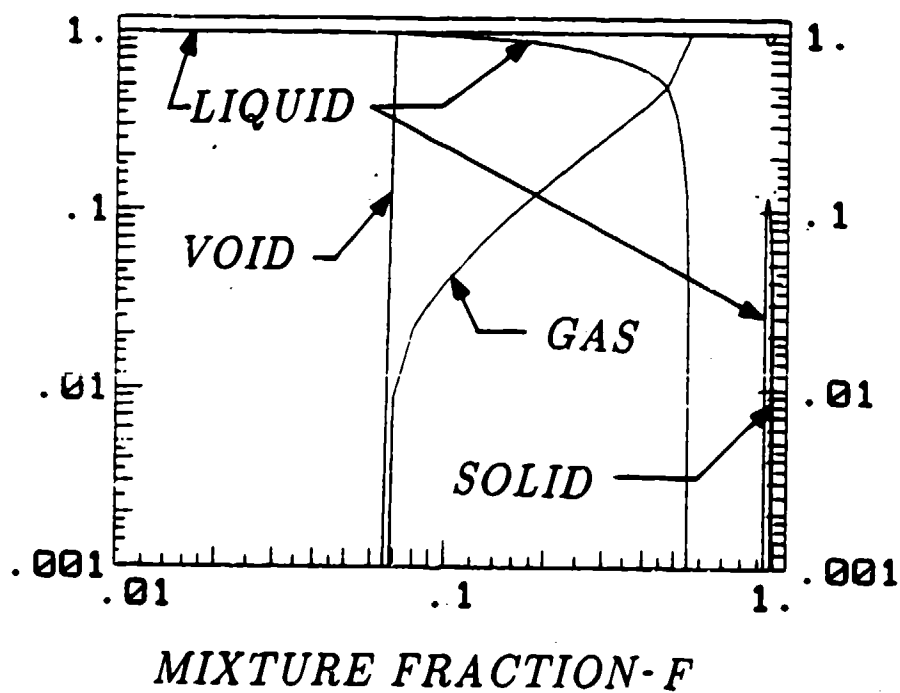
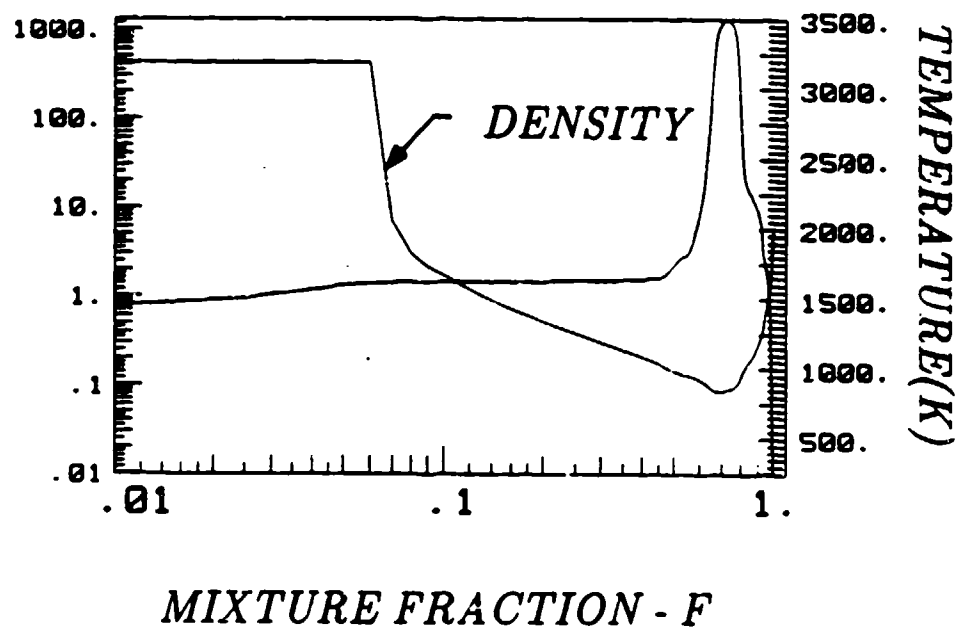


Fig.5 Equations of States For $Li - SF_6$ System with Li at 1415 K and SF_6 Gas at 298 K

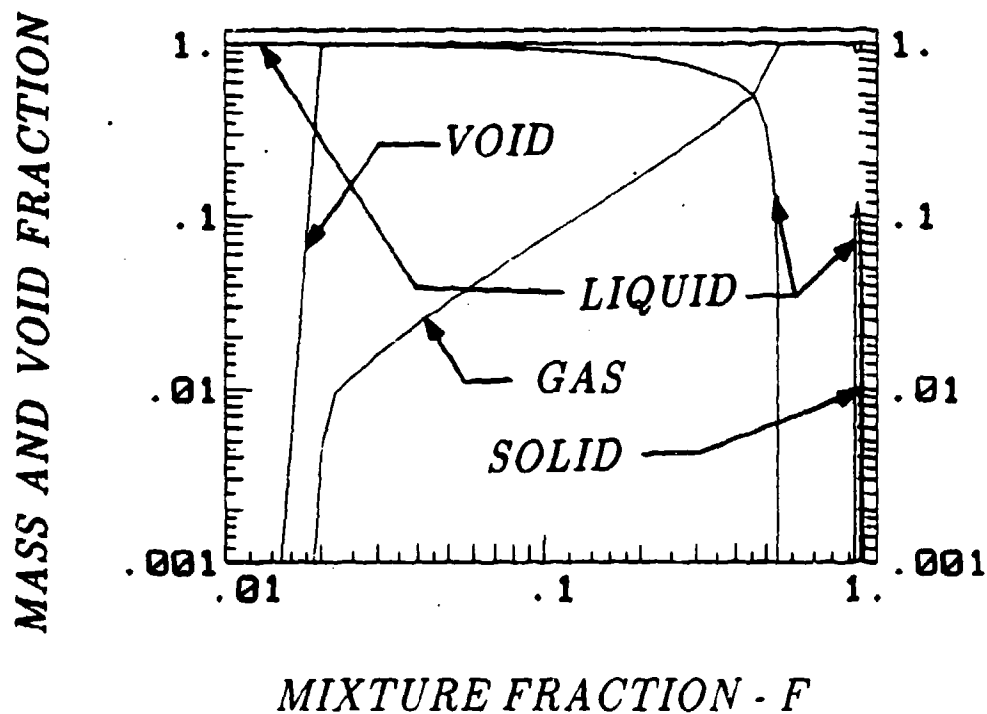
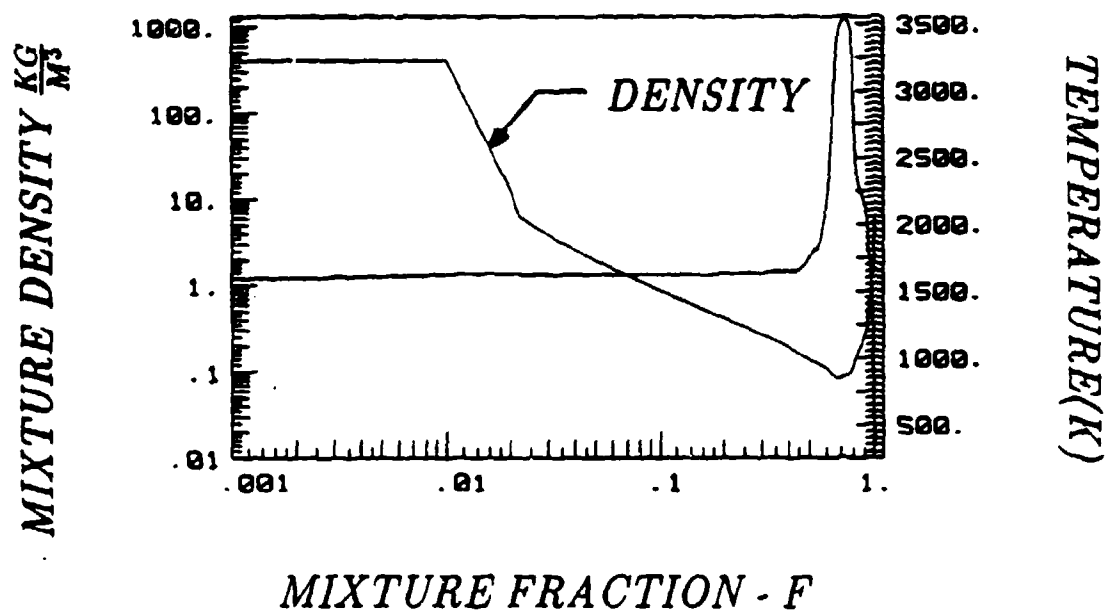


Fig.6 Equations of States For $\text{Li} - \text{SF}_6$ System with Li at 1586 K and SF_6 Gas at 298 K

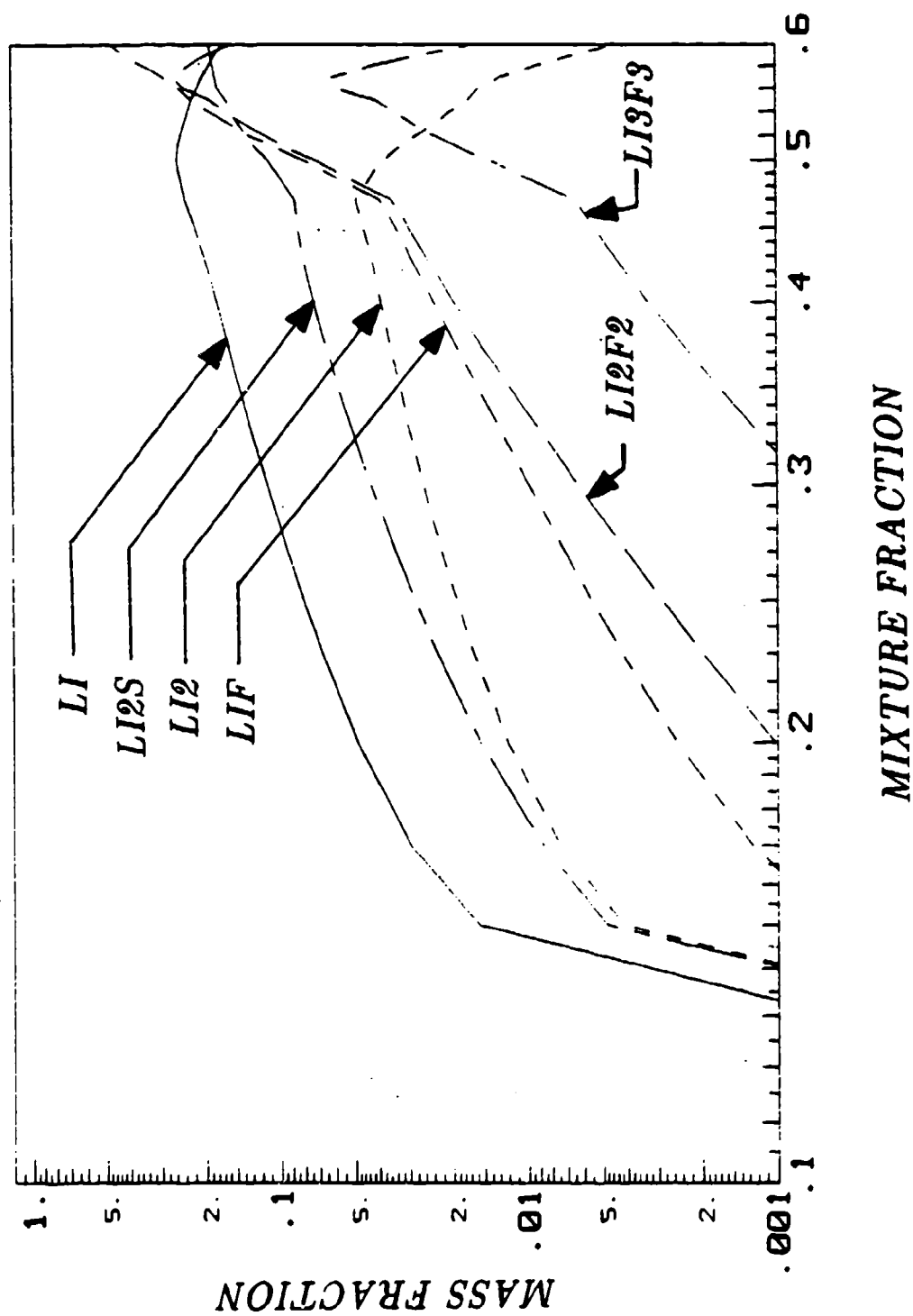


Fig. 7 Equilibrium Compositions of Li - SF₆ System with Li at 1130 K and SF₆ Gas at 298 K

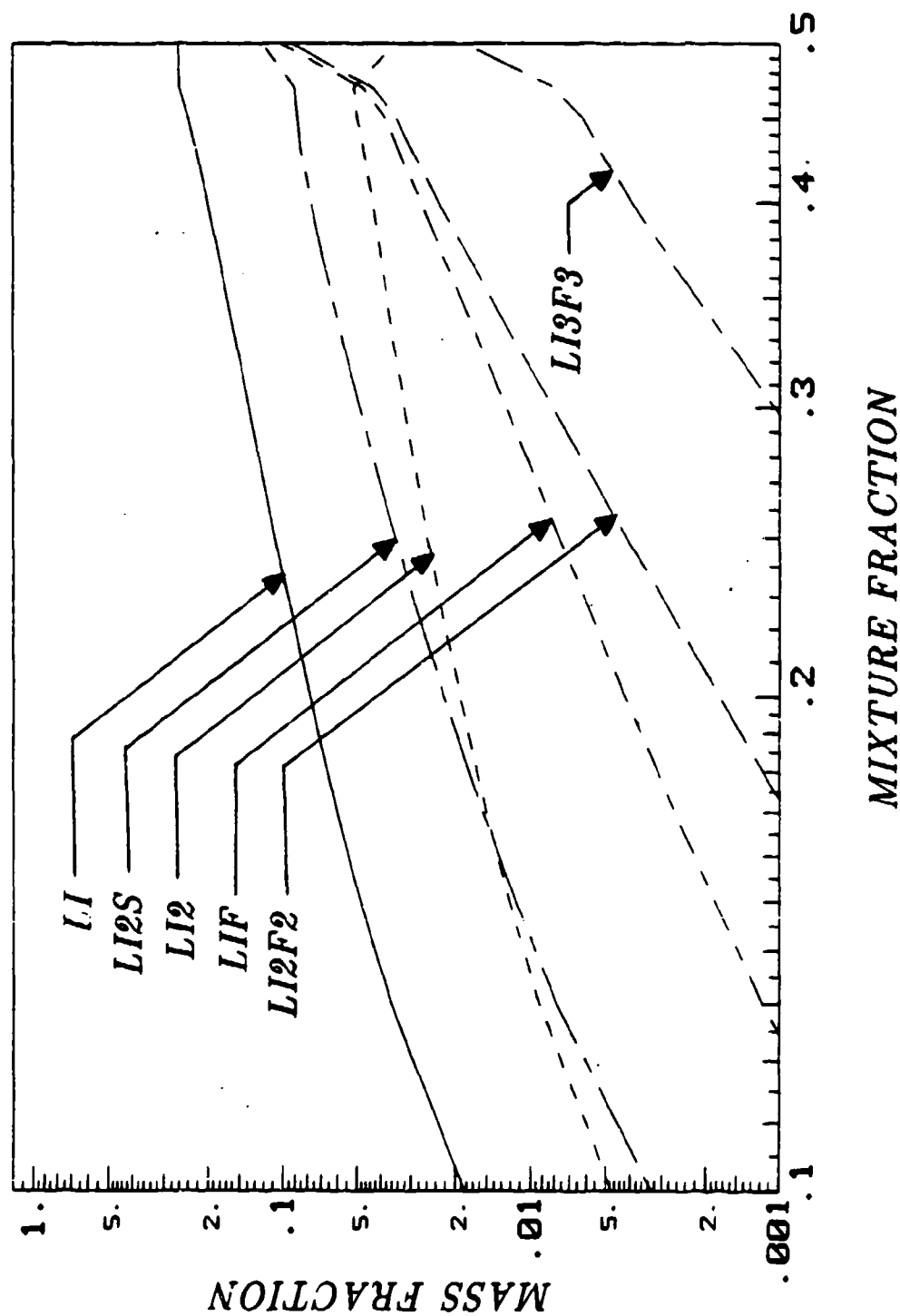


Fig.8 Equilibrium Compositions of $\text{Li} - \text{SF}_6$ System with Li at 1358 K and SF_6 Gas at 298 K

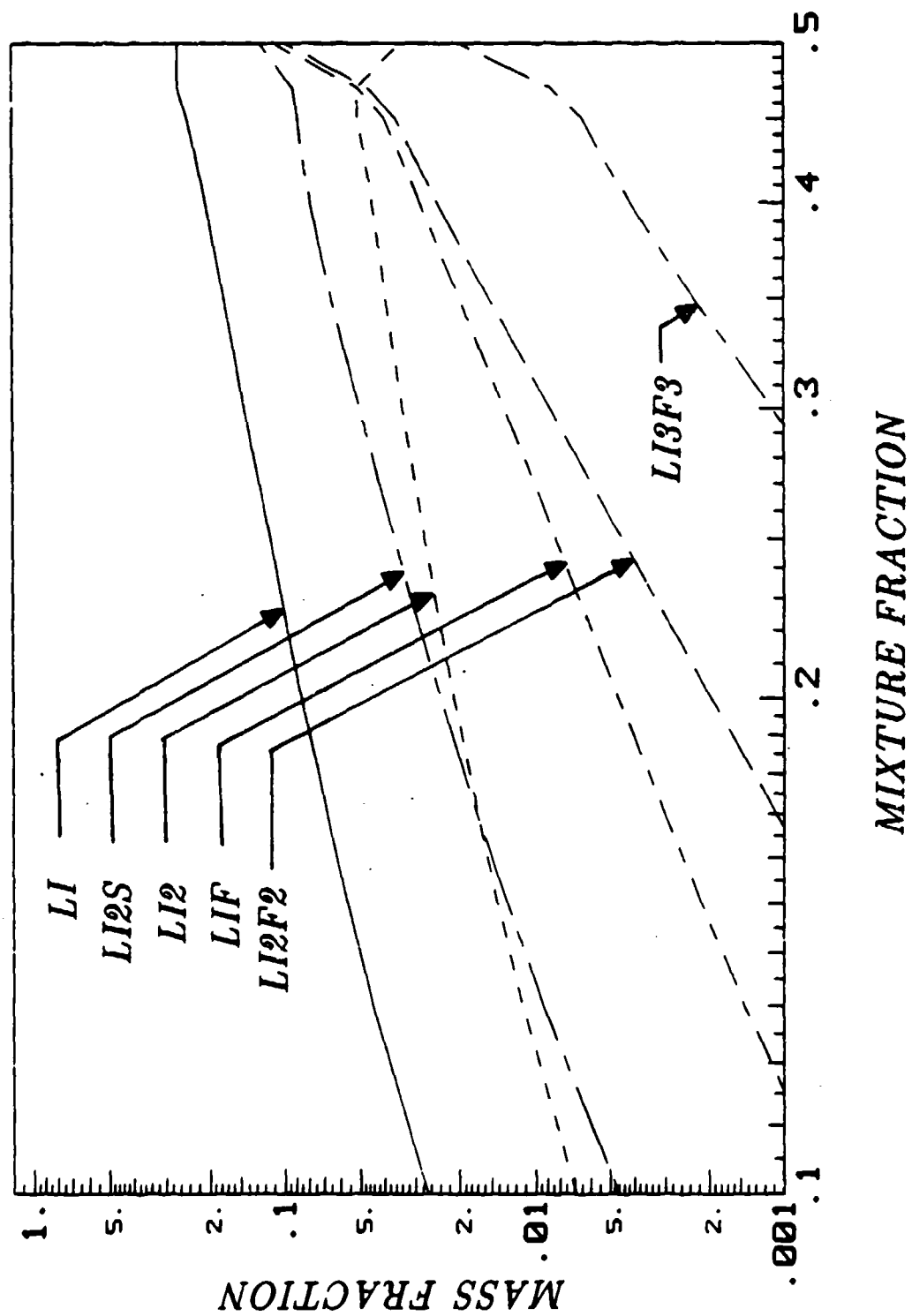


Fig.9 Equilibrium Compositions of $\text{Li} - \text{SF}_6$ System with Li at 1415 K and SF_6 Gas at 298 K

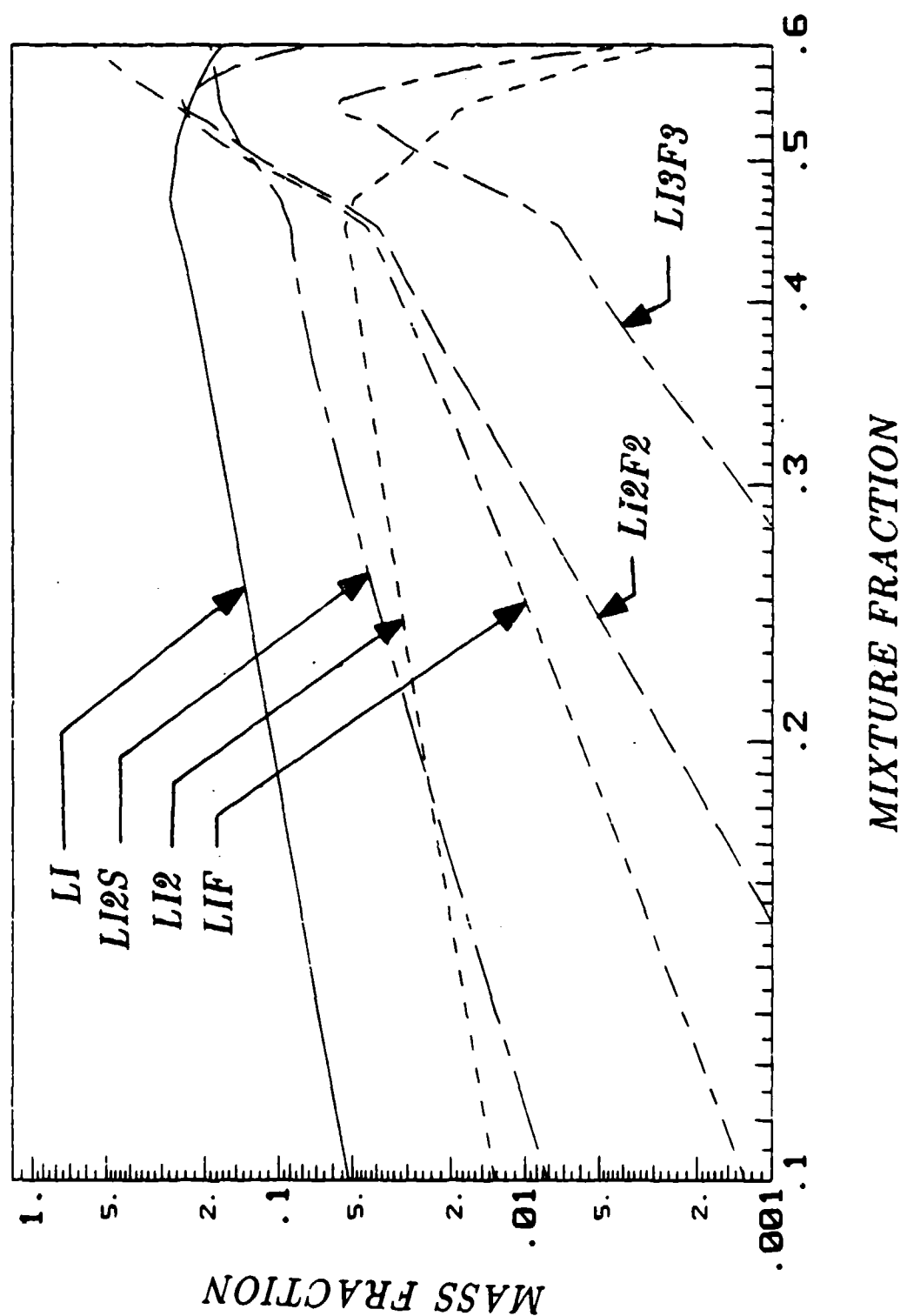
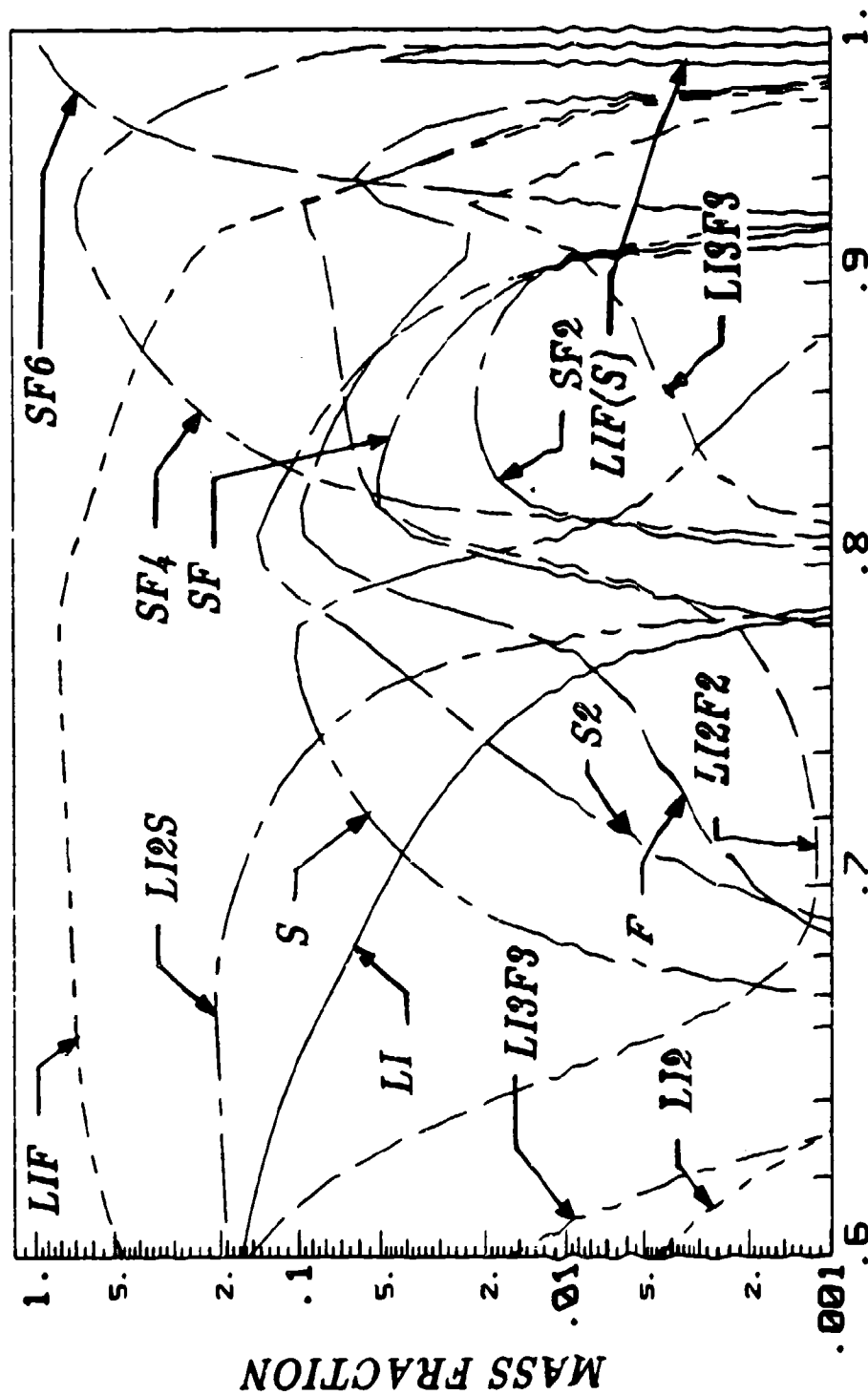
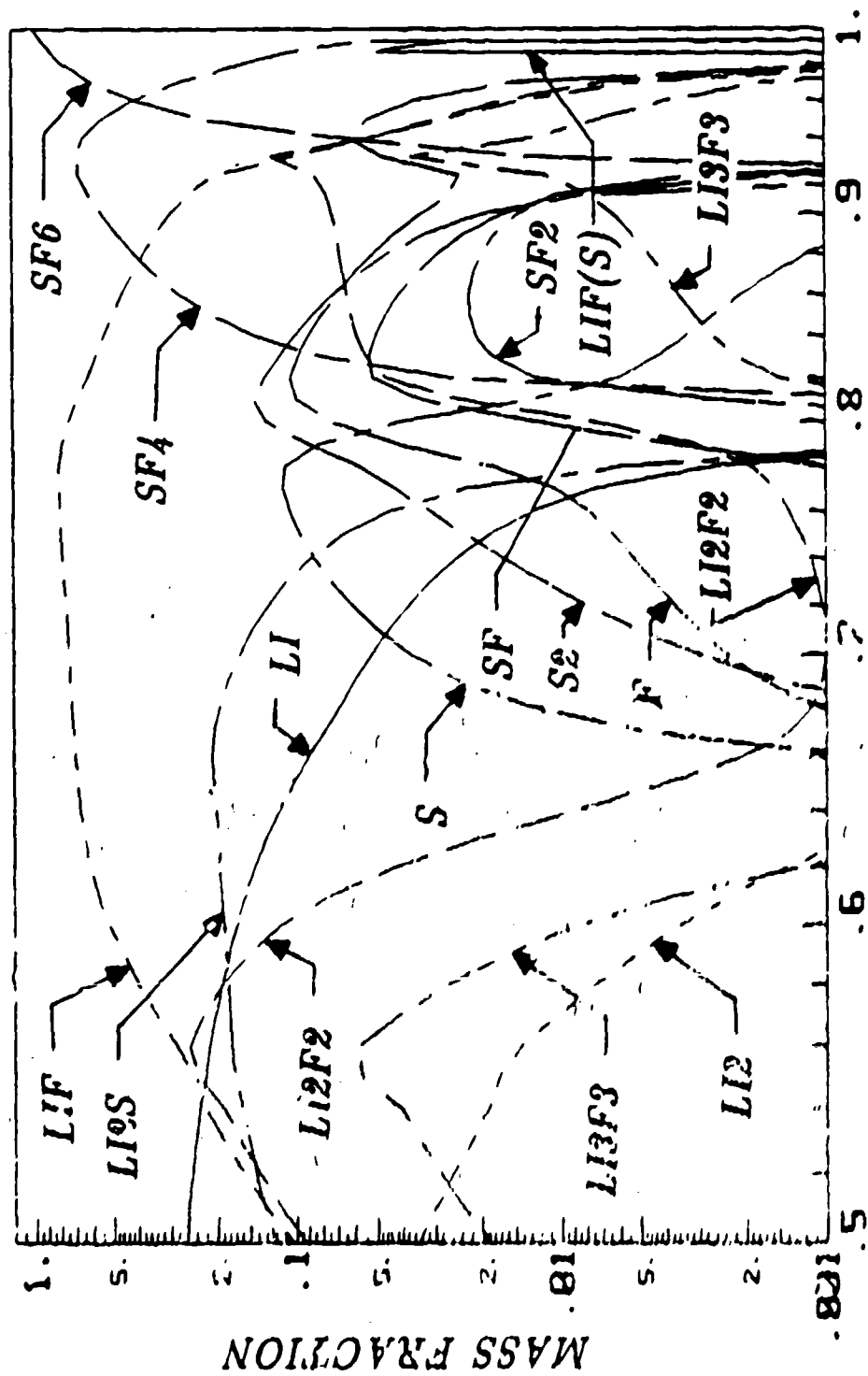


Fig.10 Equilibrium Compositions of $\text{Li}-\text{SF}_6$ System with Li at 1586 K and SF_6 Gas at 298 K



MIXTURE FRACTION

Fig.11 Equilibrium Compositions of Li - SF₆ System with Li at 1130 K and SF₆ Gas at 298 K



MIXTURE FRACTION

Fig. 12 Liquidus Composition of $\text{Li}-\text{SF}_6$ System with Li at 1358 K and SF_6 Gas at 298 K

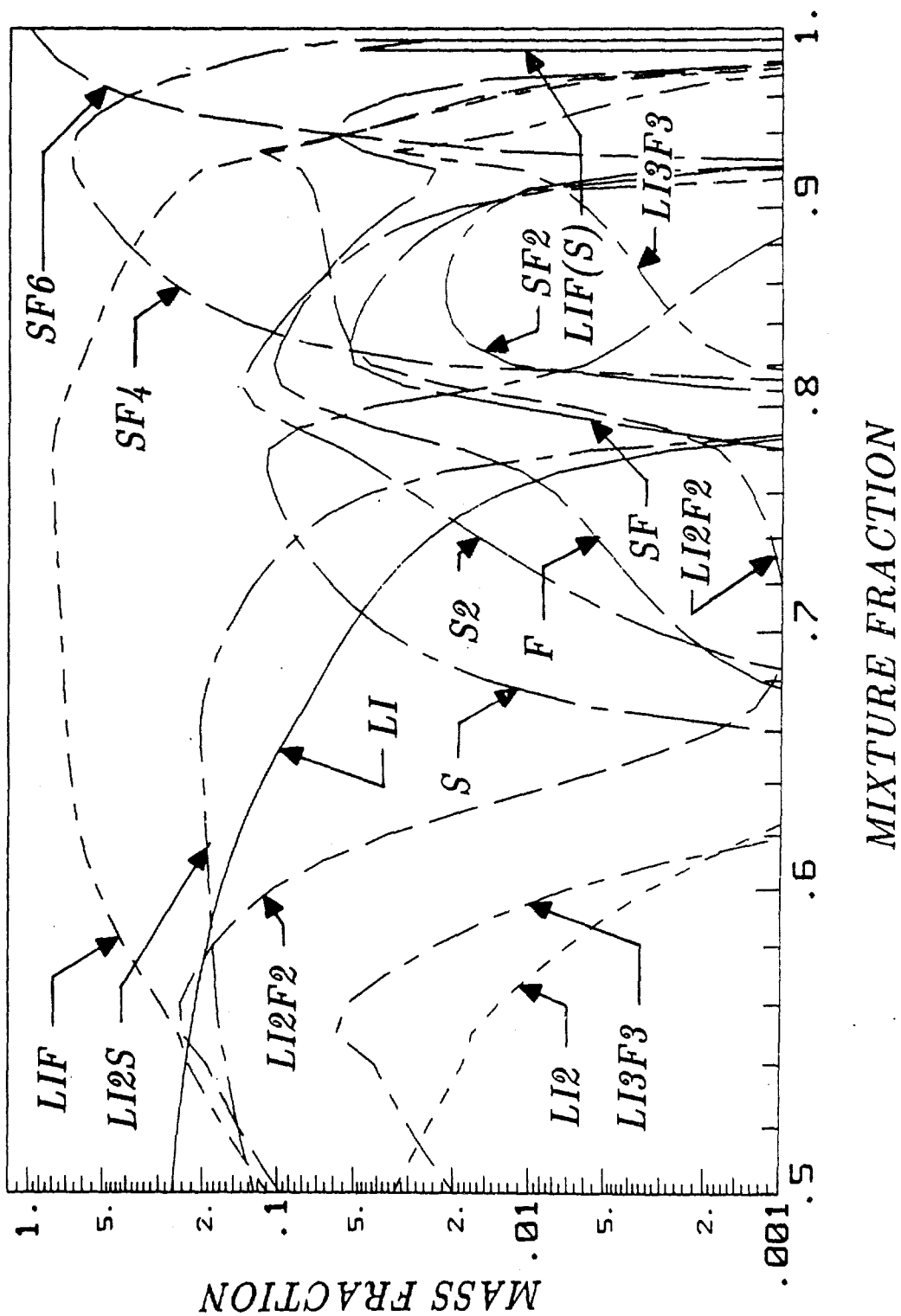
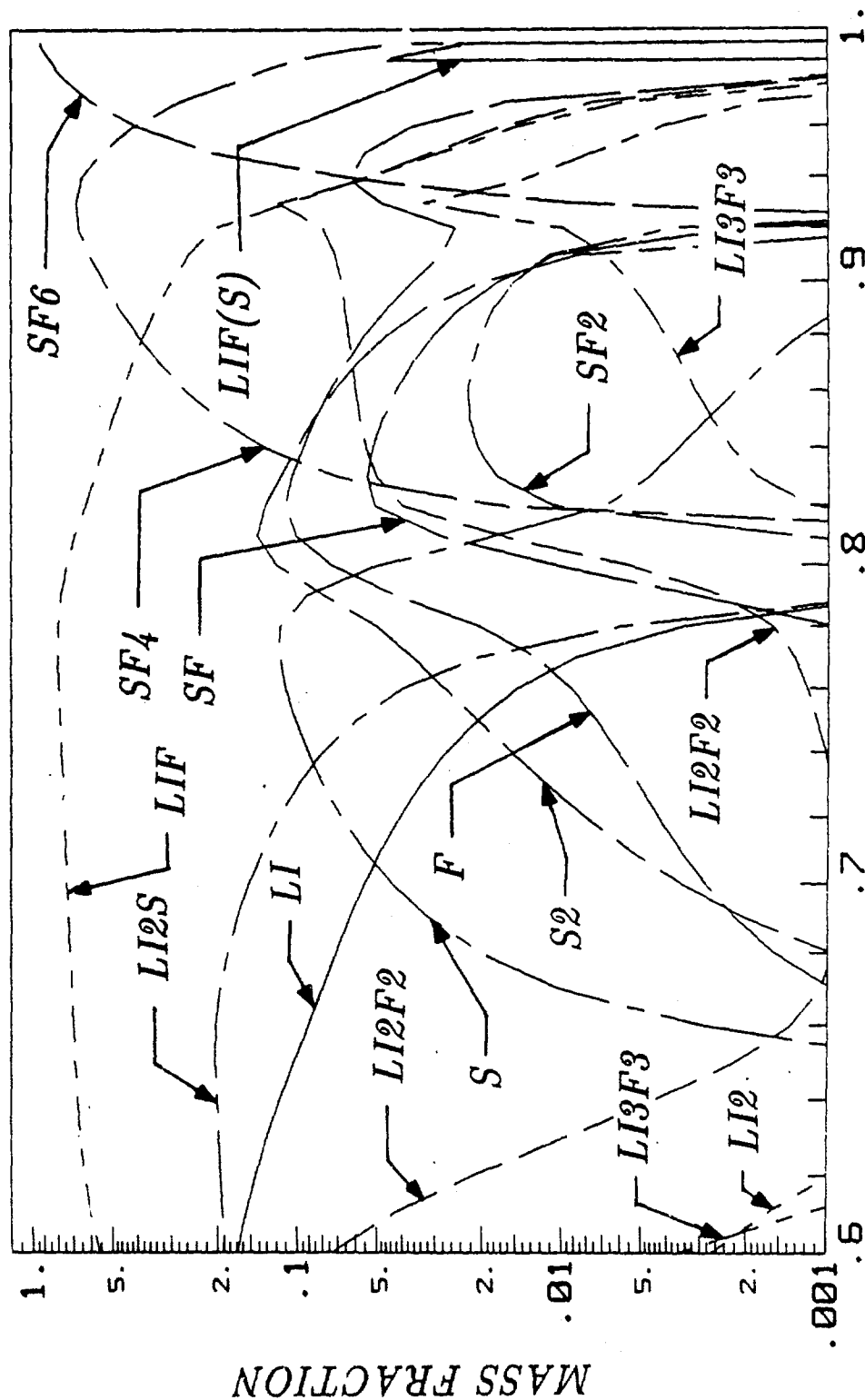


Fig.13 Equilibrium Compositions of $\text{Li}-\text{SF}_6$ System with Li at 1415 K and SF_6 Gas at 298 K



MIXTURE FRACTION

Fig.14 Equilibrium Compositions of $\text{Li}-\text{SF}_6$ System with Li at 1586 K and SF_6 Gas at 298 K

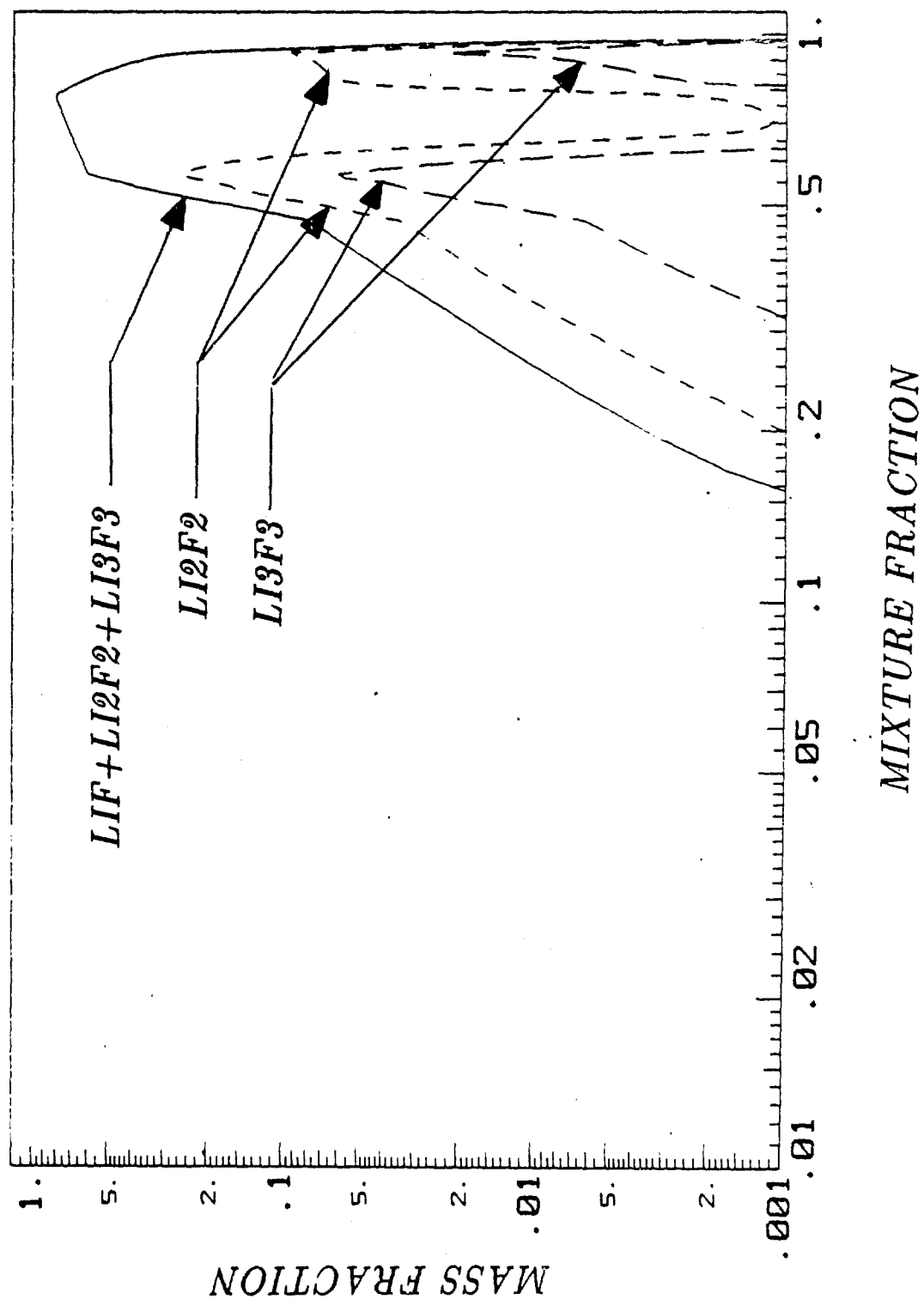


Fig.15 Equilibrium Compositions of $\text{Li} - \text{SF}_6$ System with Li at 1130 K and SF_6 Gas at 298 K

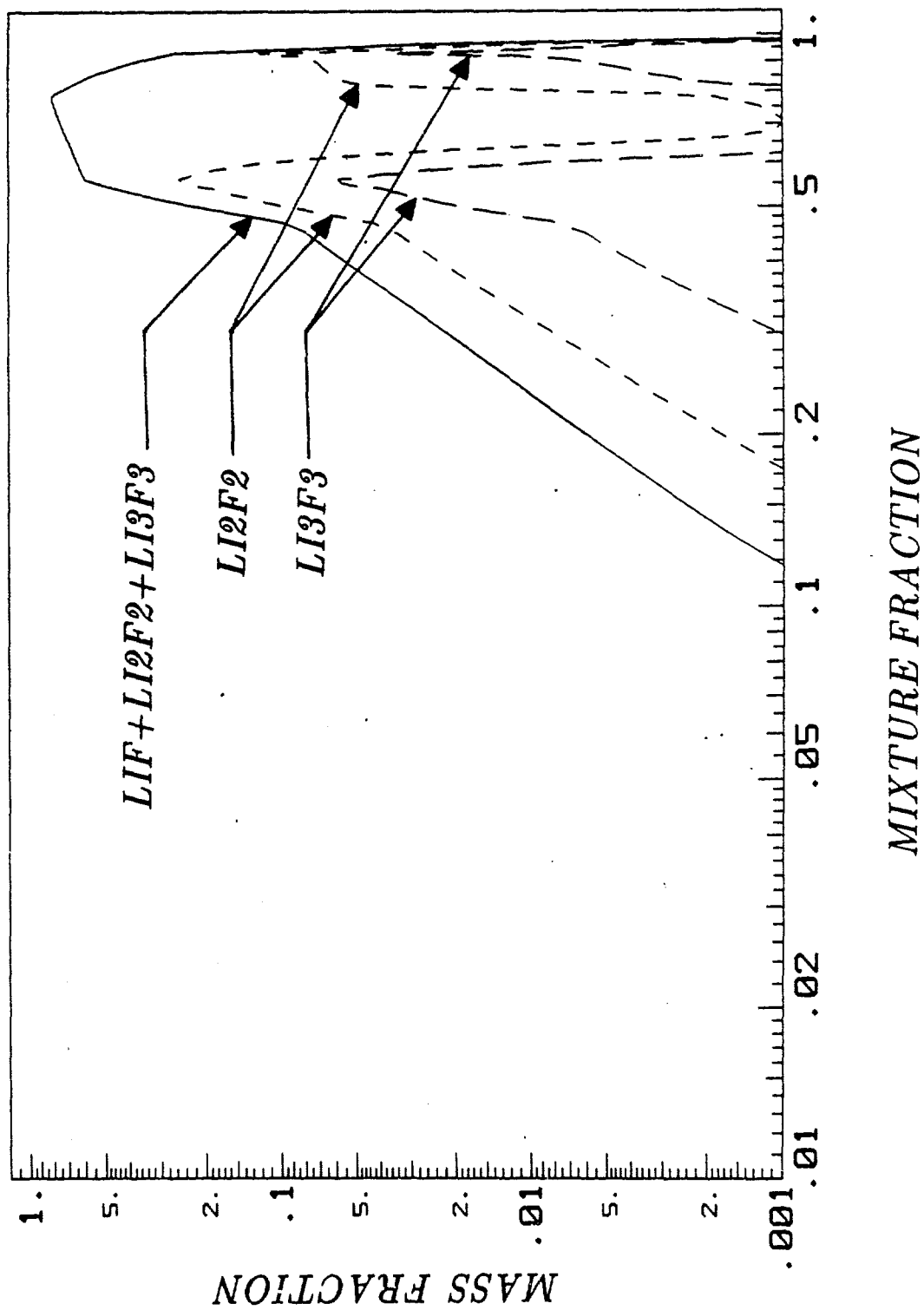


Fig.16 Equilibrium Compositions of $\text{Li}-\text{SF}_6$ System with Li at 1358 K and SF_6 Gas at 298 K

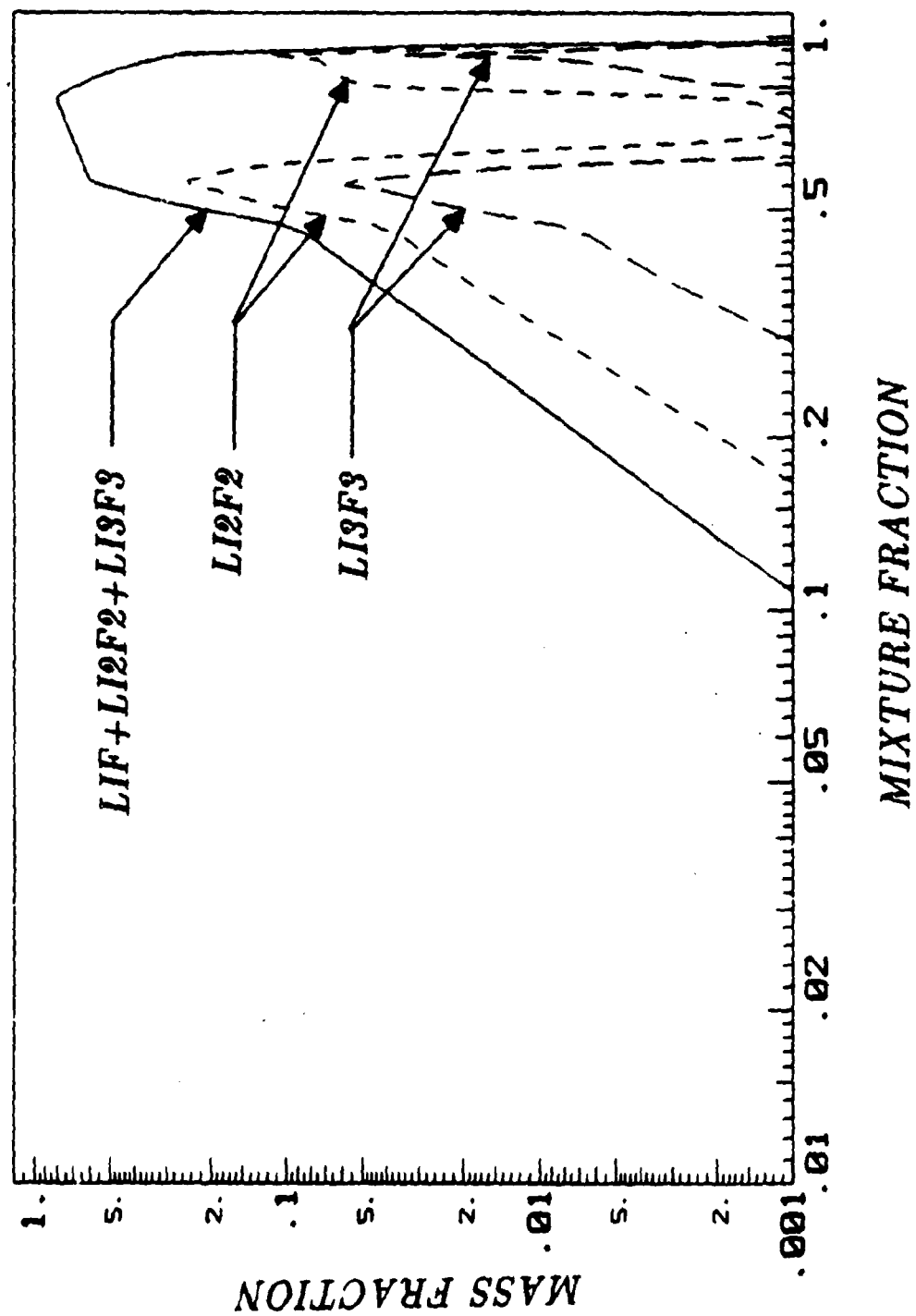


Fig.17 Equilibrium Compositions of $\text{Li}-\text{SF}_6$ System with Li at 1415 K and SF_6 Gas at 298 K

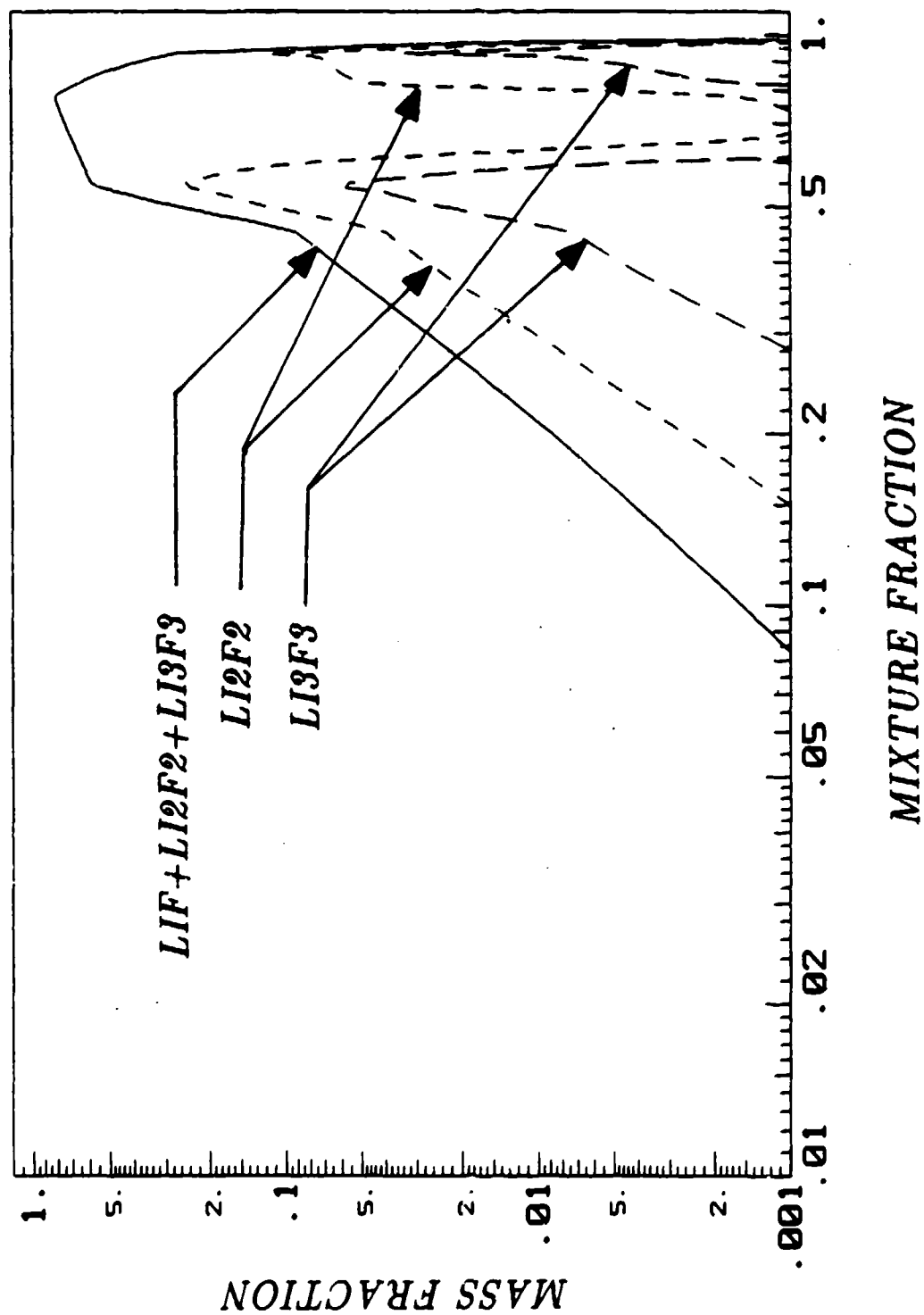
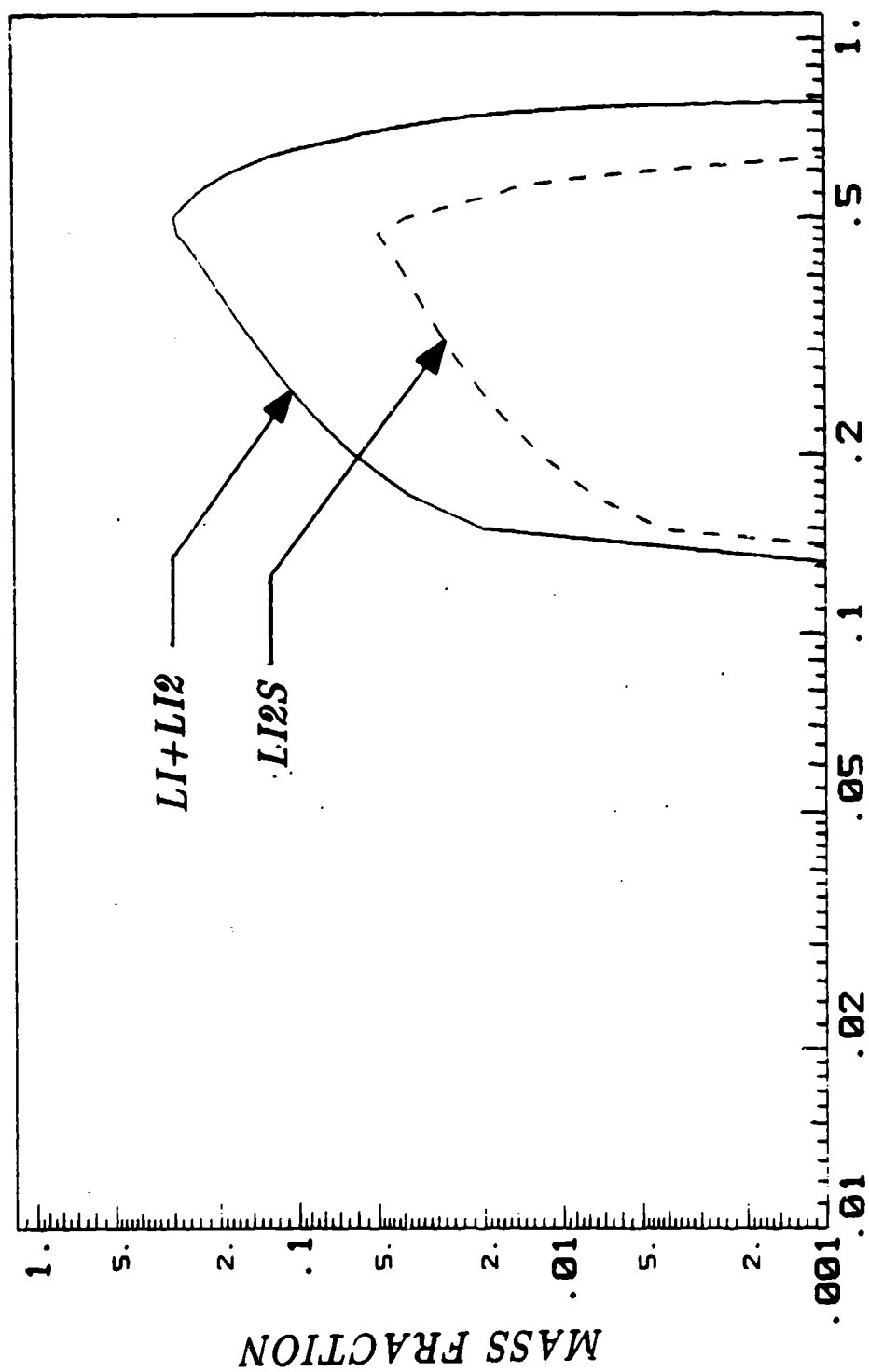


Fig. 18 Equilibrium Compositions of $\text{Li}-\text{SF}_6$ System with Li at 1586 K and SF_6 Gas at 298 K



MIXTURE FRACTION

Fig.19 Equilibrium Compositions of Li - SF₆ System with Li at 1130 K and SF₆ Gas at 298 K

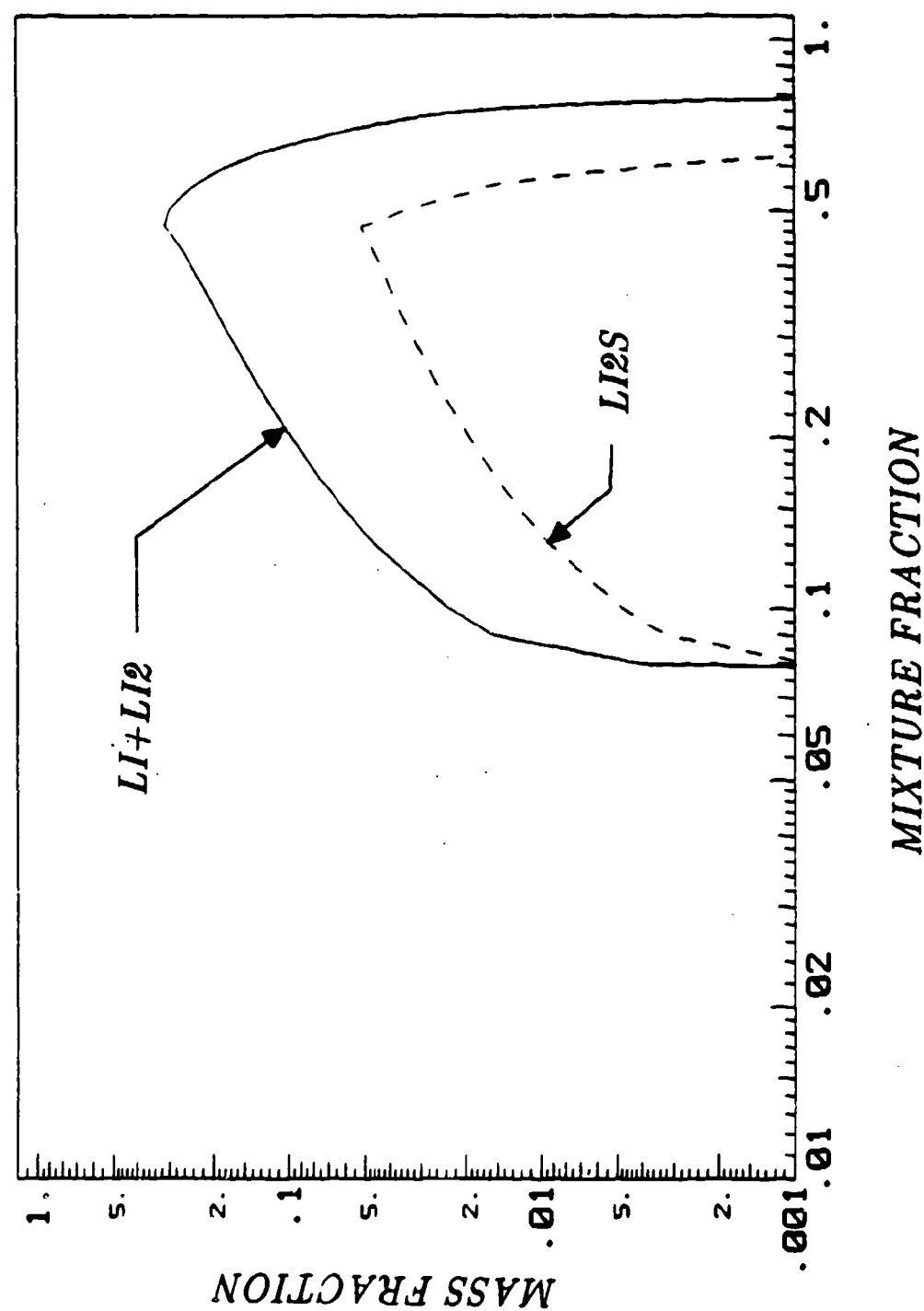


Fig.20 Equilibrium Compositions of Li - SF₆ System with Li at 1358 K and SF₆ Gas at 298 K

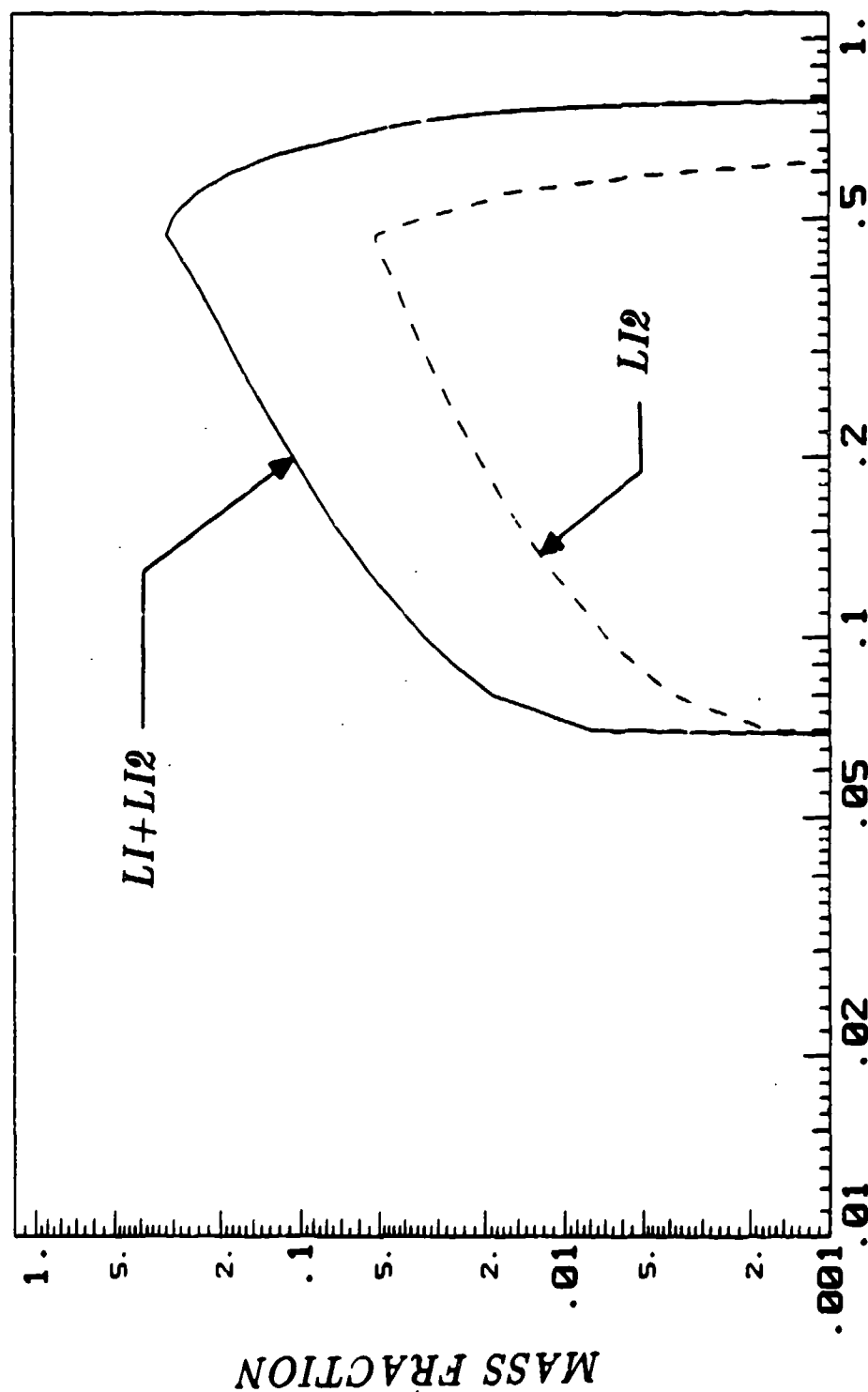


Fig.21 Equilibrium Compositions of Li - SF₆ System with Li at 1415 K and SF₆ Gas at 298 K

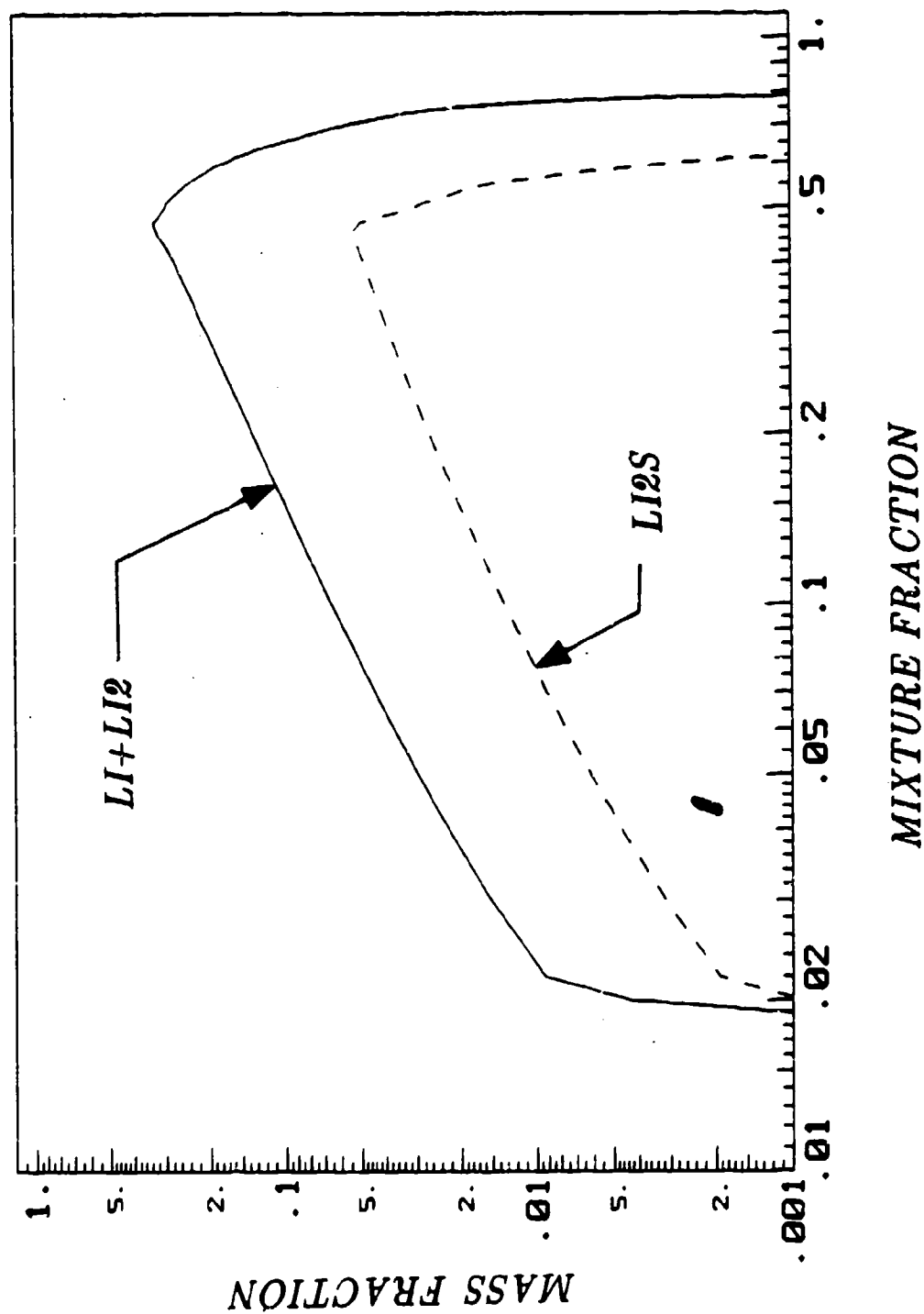


Fig.22 Equilibrium Compositions of Li - SF₆ System with Li at 1586 K and SF₆ Gas at 298 K

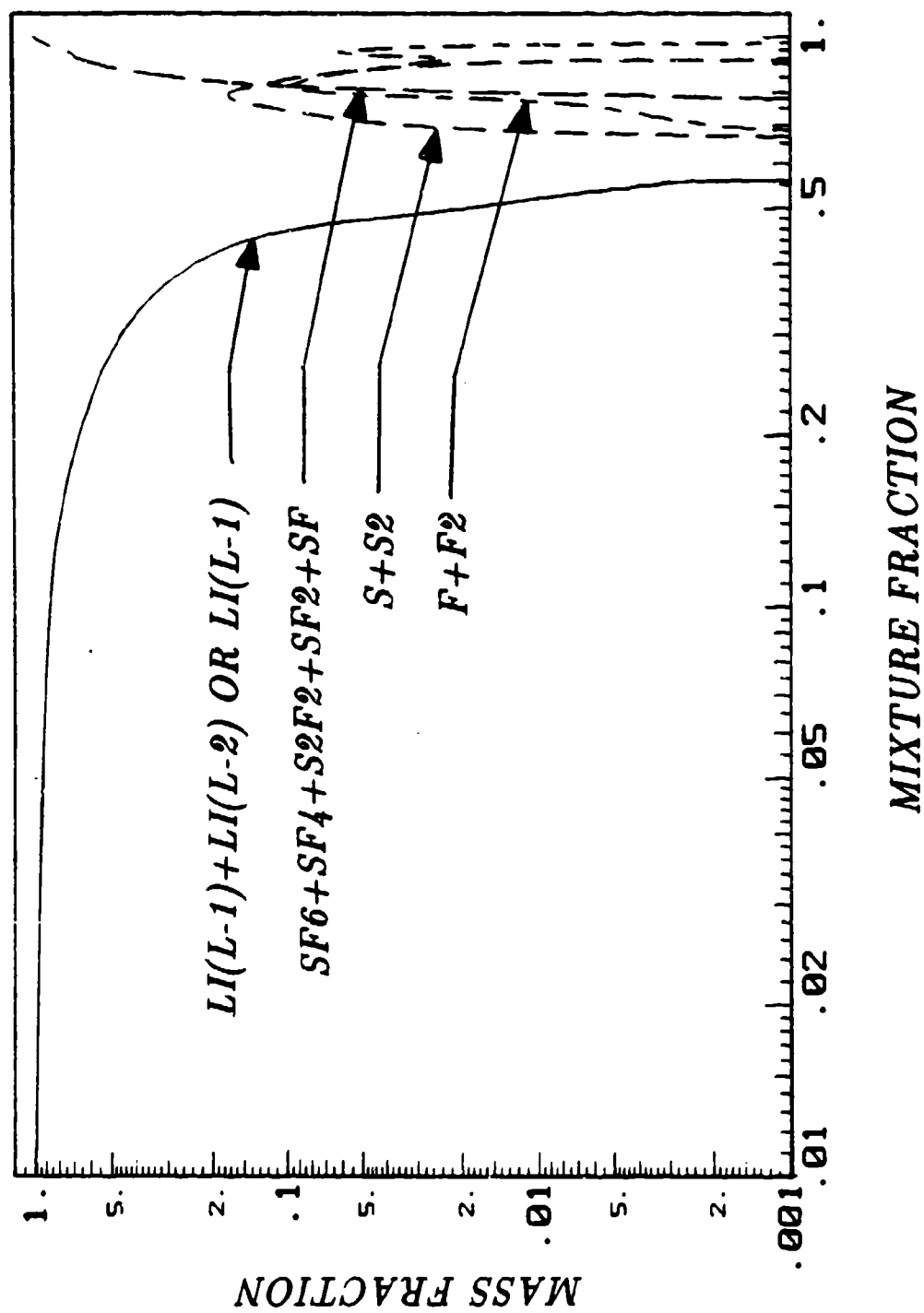


Fig.23 Equilibrium Compositions of Li - SF₆ System with Li at 1130 K and SF₆ Gas at 298 K

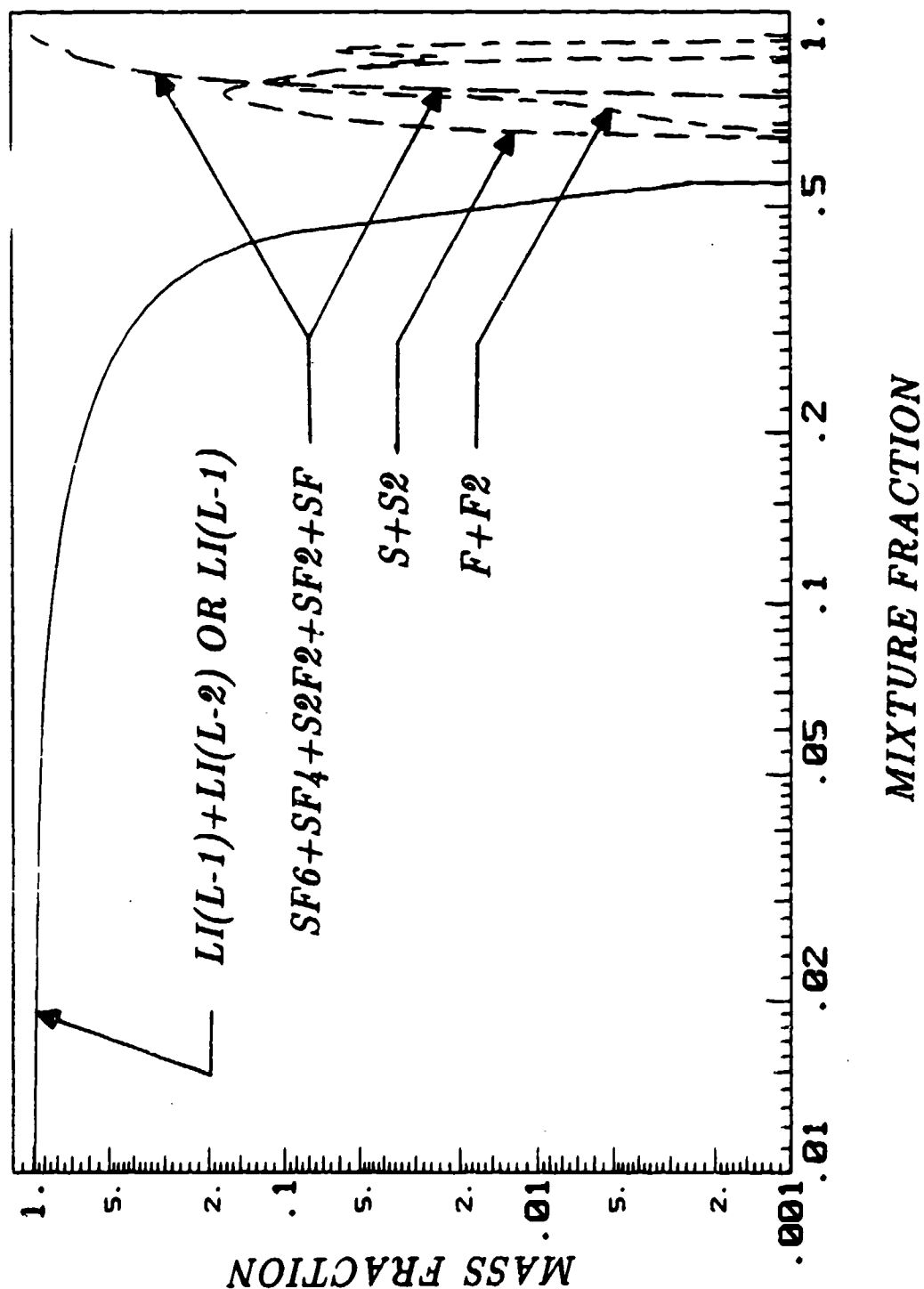


Fig.24 Equilibrium Compositions of $\text{Li} - \text{SF}_6$ System with Li at 1358 K and SF_6 Gas at 298 K

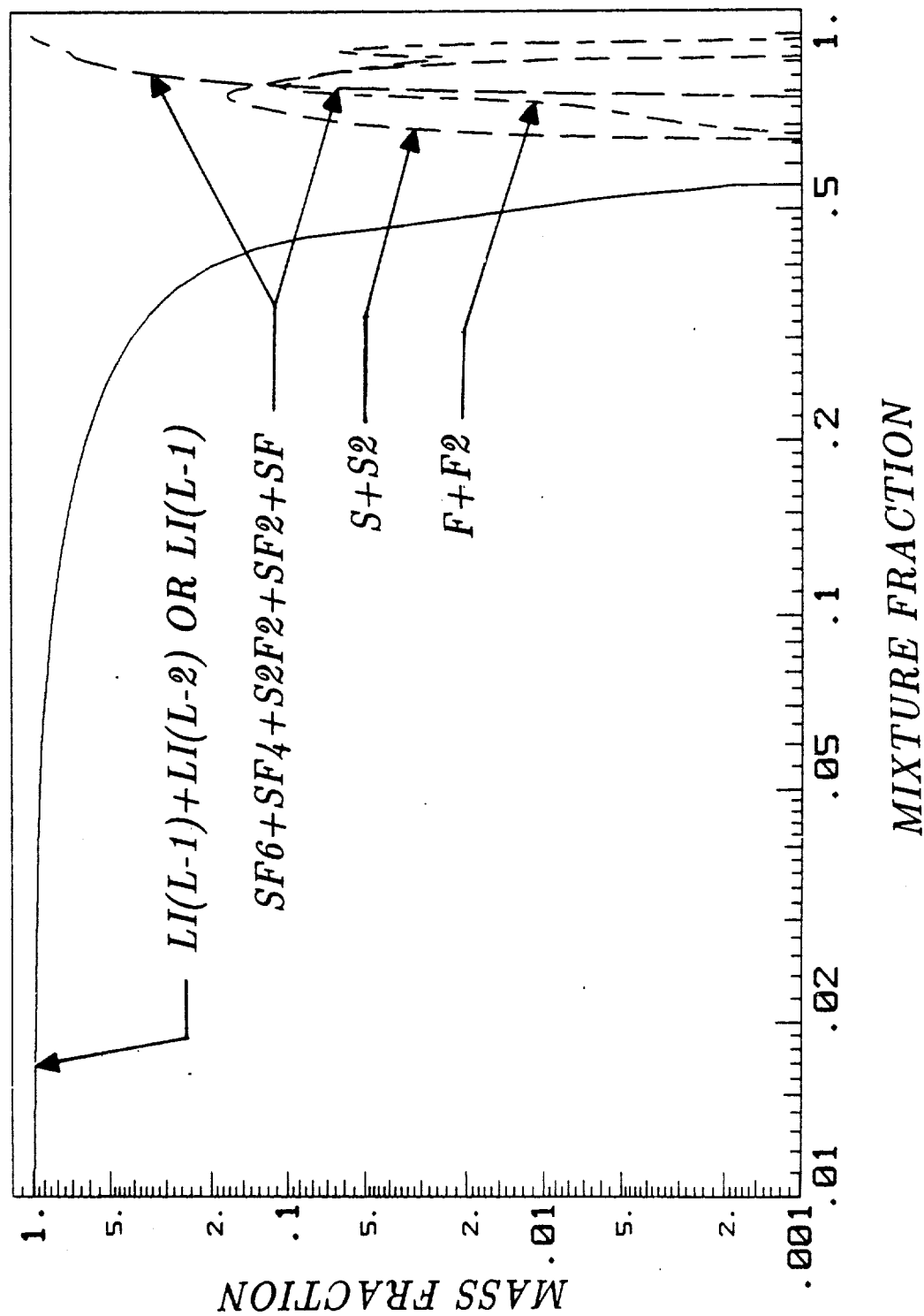


Fig.25 Equilibrium Compositions of $Li - SF_6$ System with Li at 1415 K and SF_6 Gas at 298 K

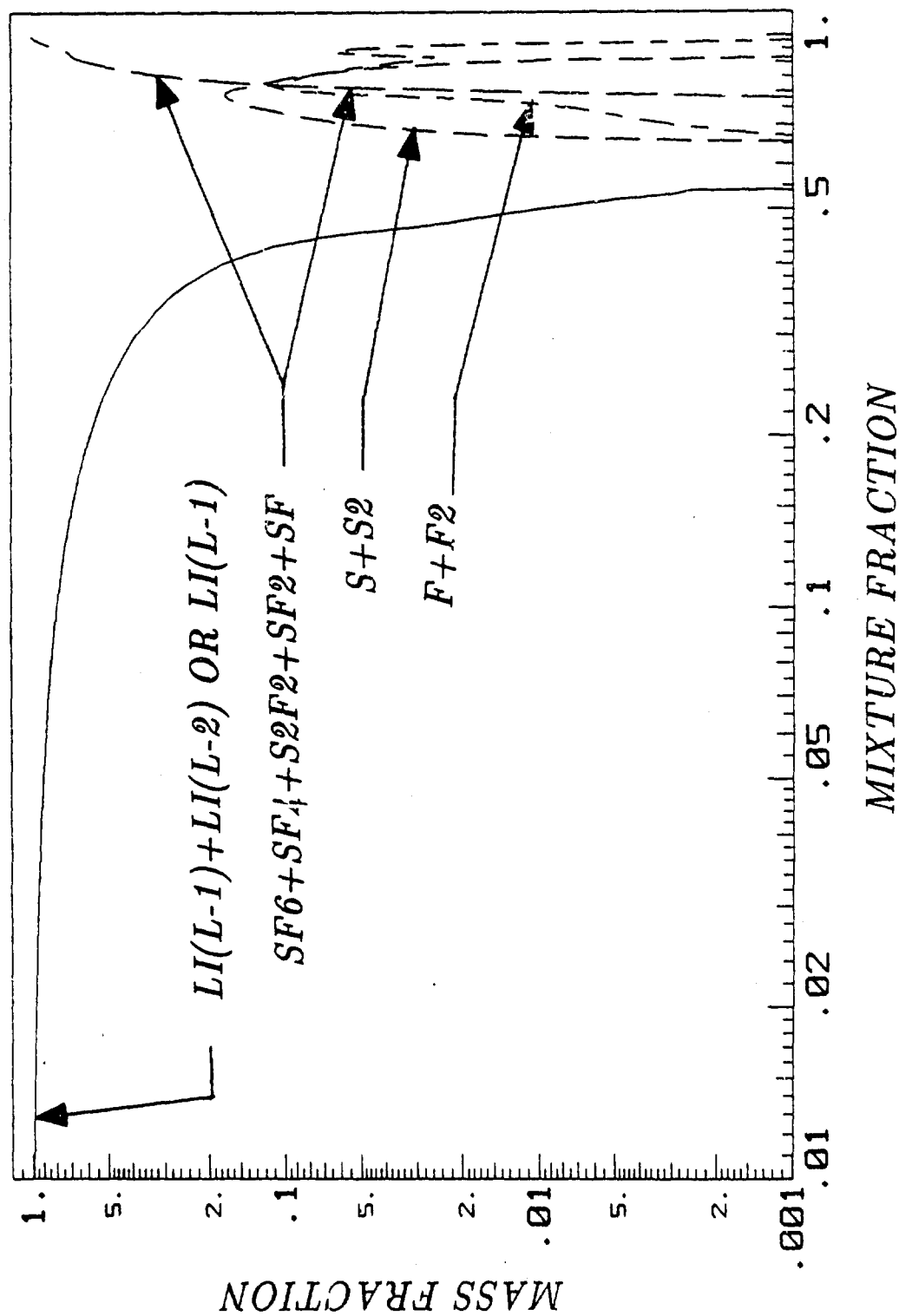
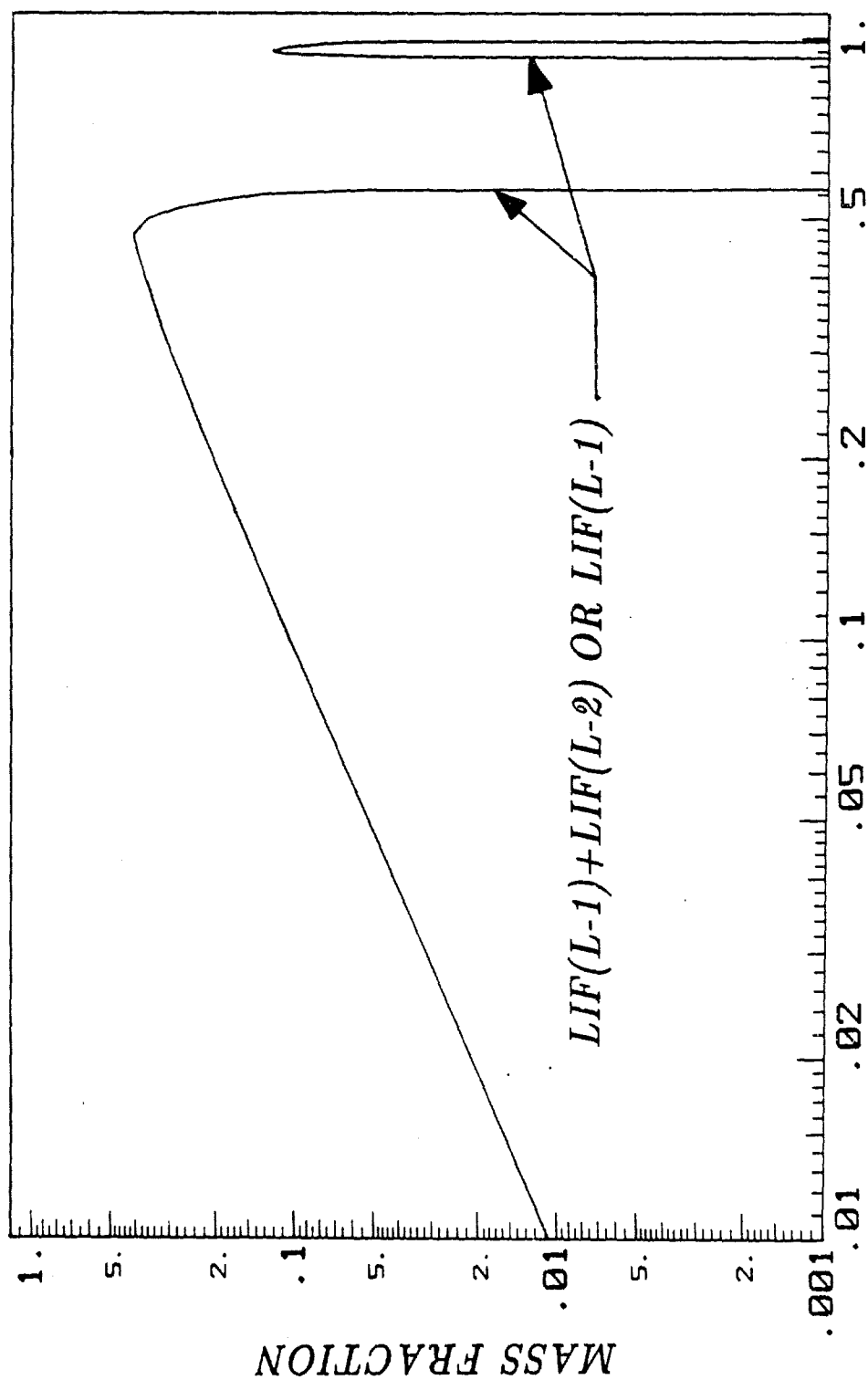


Fig.26 Equilibrium Compositions of *Li* - *SF*₆ System with *Li* at 1586 K and *SF*₆ Gas at 298 K



MIXTURE FRACTION

Fig.27 Equilibrium Compositions of $\text{Li}-\text{SF}_6$ System with Li at 1130 K and SF_6 Gas at 298 K

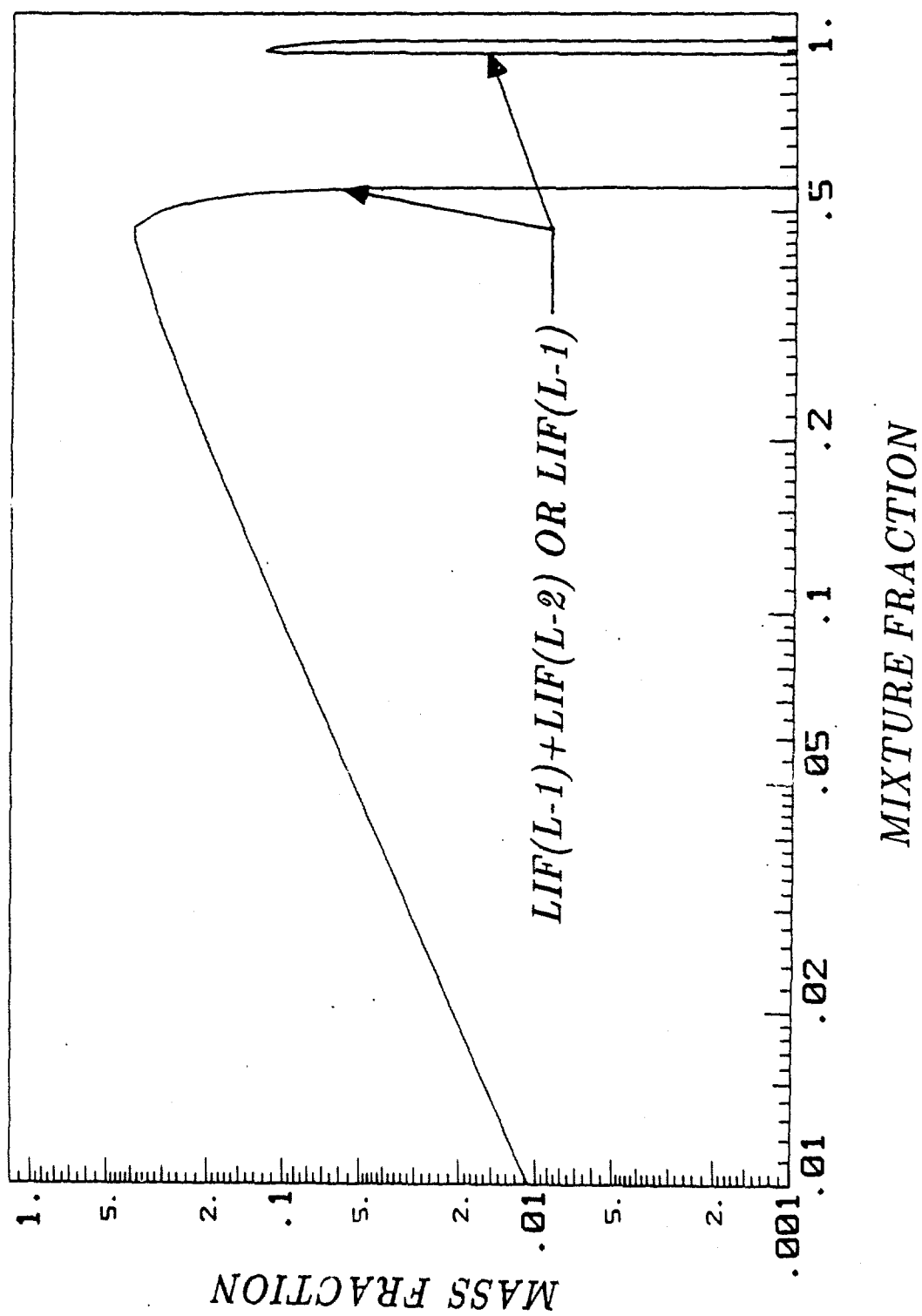


Fig.28 Equilibrium Compositions of *Li* - *SF*₆ System with *Li* at 1358 K and *SF*₆ Gas at 298 K

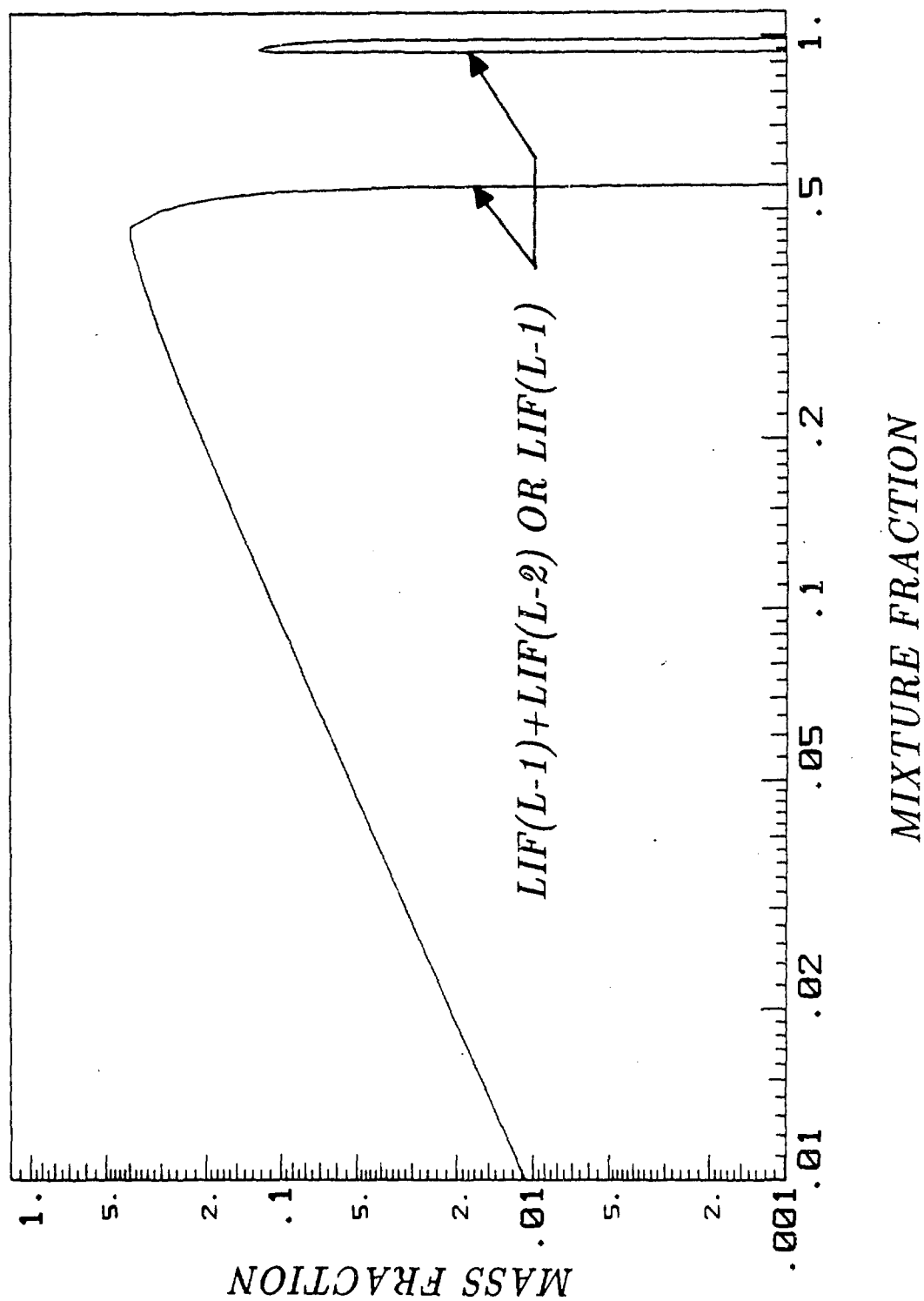


Fig.29 Equilibrium Compositions of $Li - SF_6$ System with Li at 1415 K and SF_6 Gas at 298 K

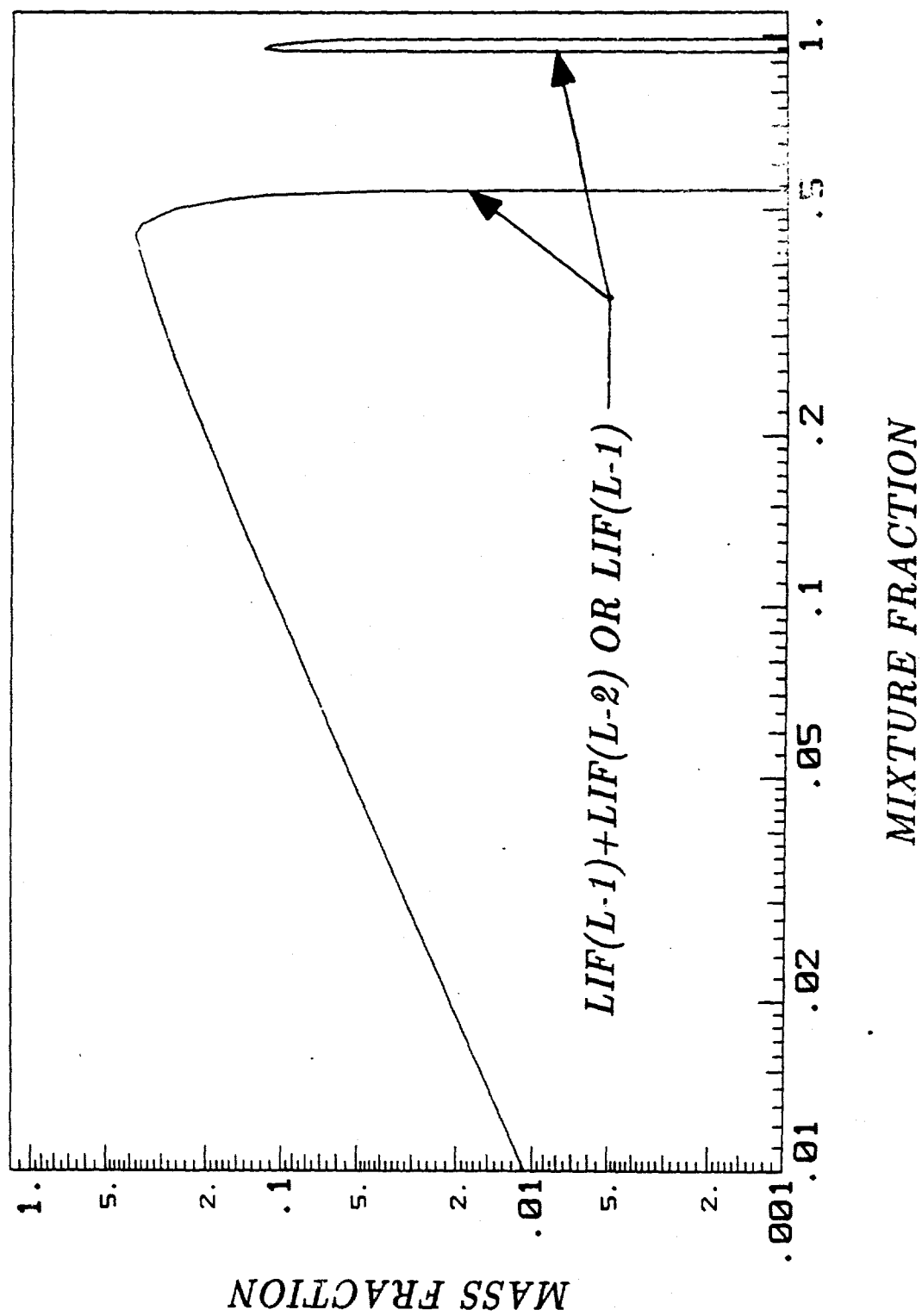


Fig.30 Equilibrium Compositions of $Li - SF_6$ System with Li at 1586 K and SF_6 Gas at 298 K

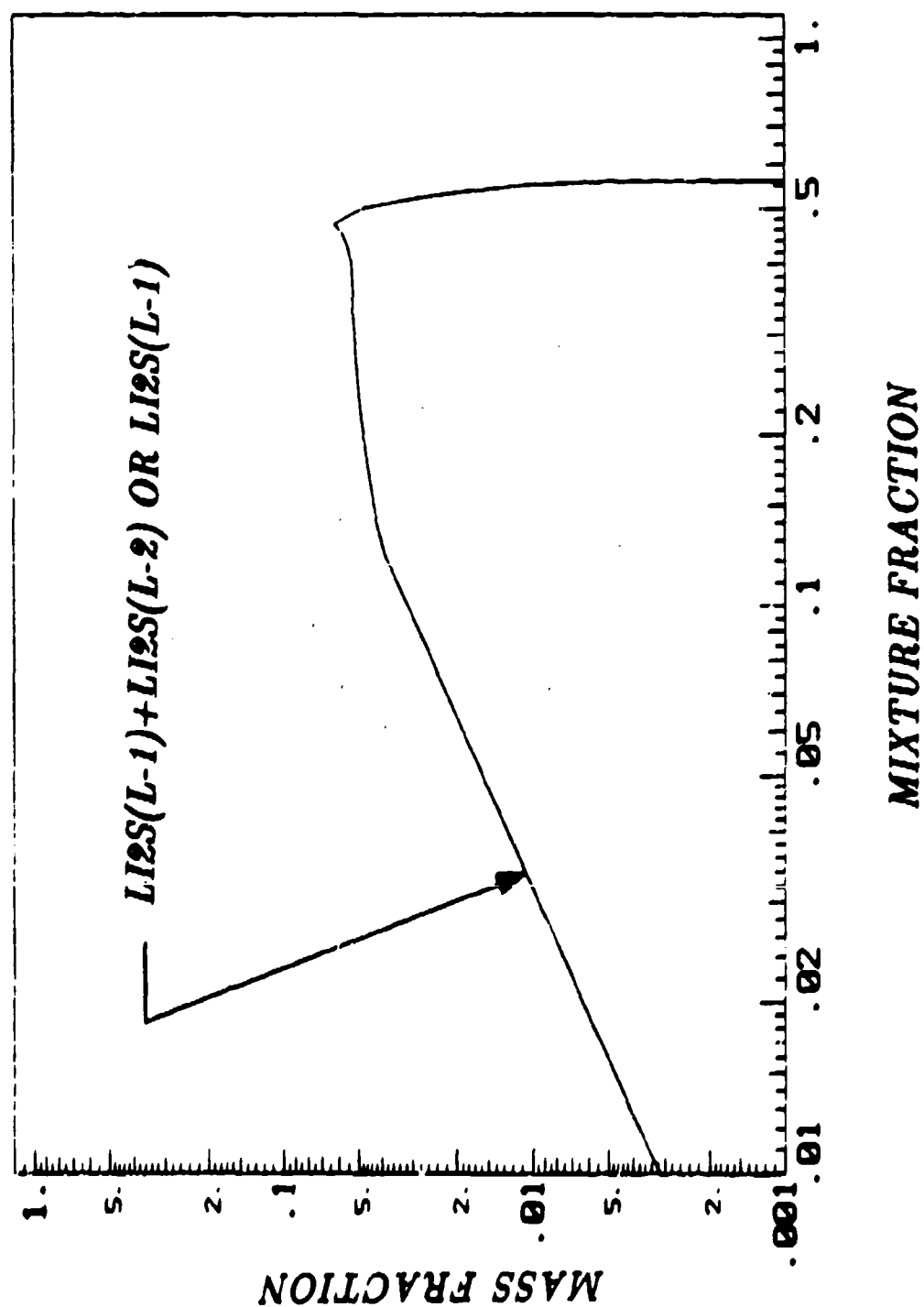


Fig.31 Equilibrium Compositions of Li - SF_6 System with Li at 1130 K and SF_6 Gas at 298 K

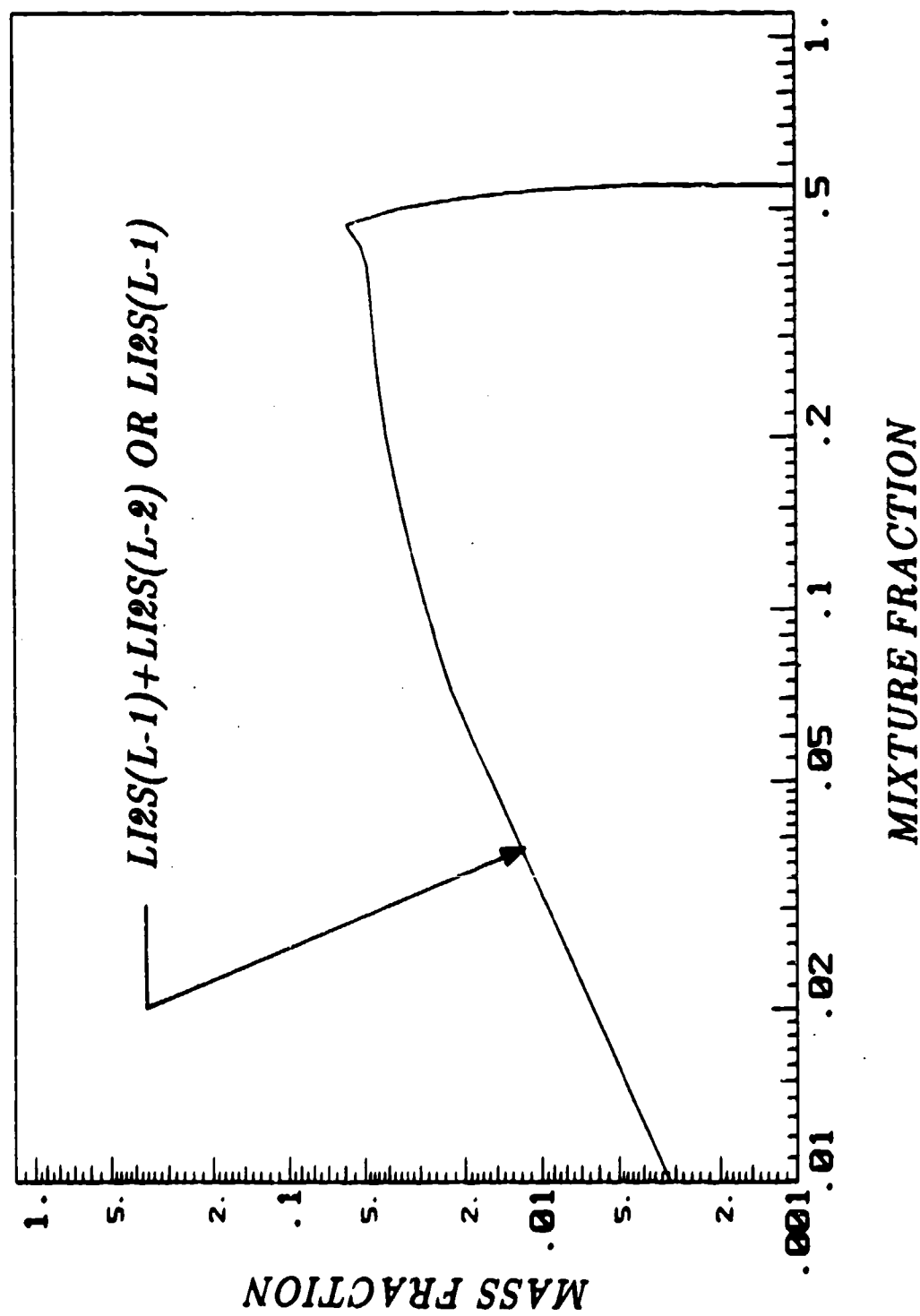


Fig. 32 Equilibrium Compositions of Li - SF_6 System with Li at 1358 K and SF_6 Gas at 298 K

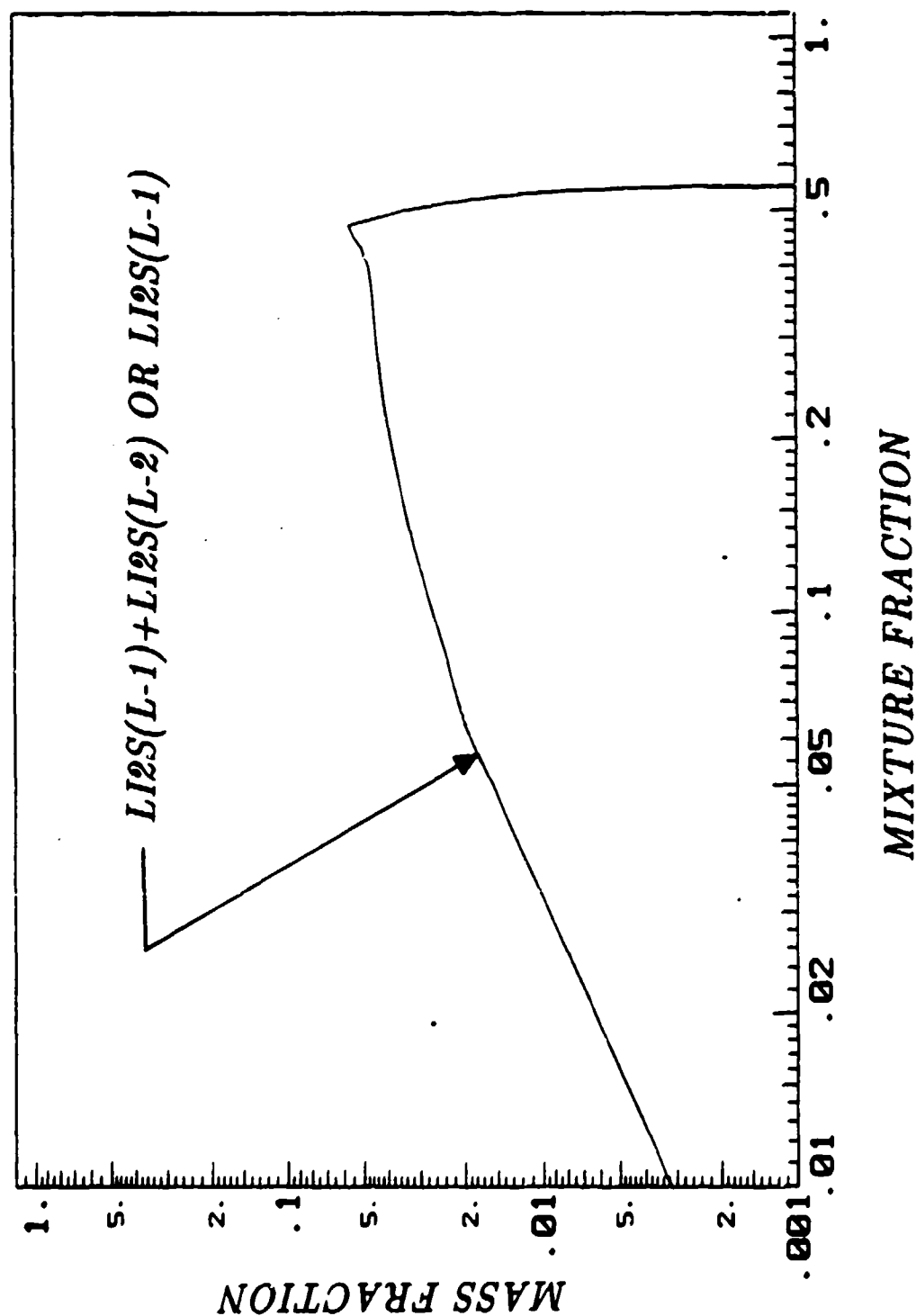


Fig.33 Equilibrium Compositions of $\text{Li} - \text{SF}_6$ System with Li at 1415 K and SF_6 Gas at 298 K

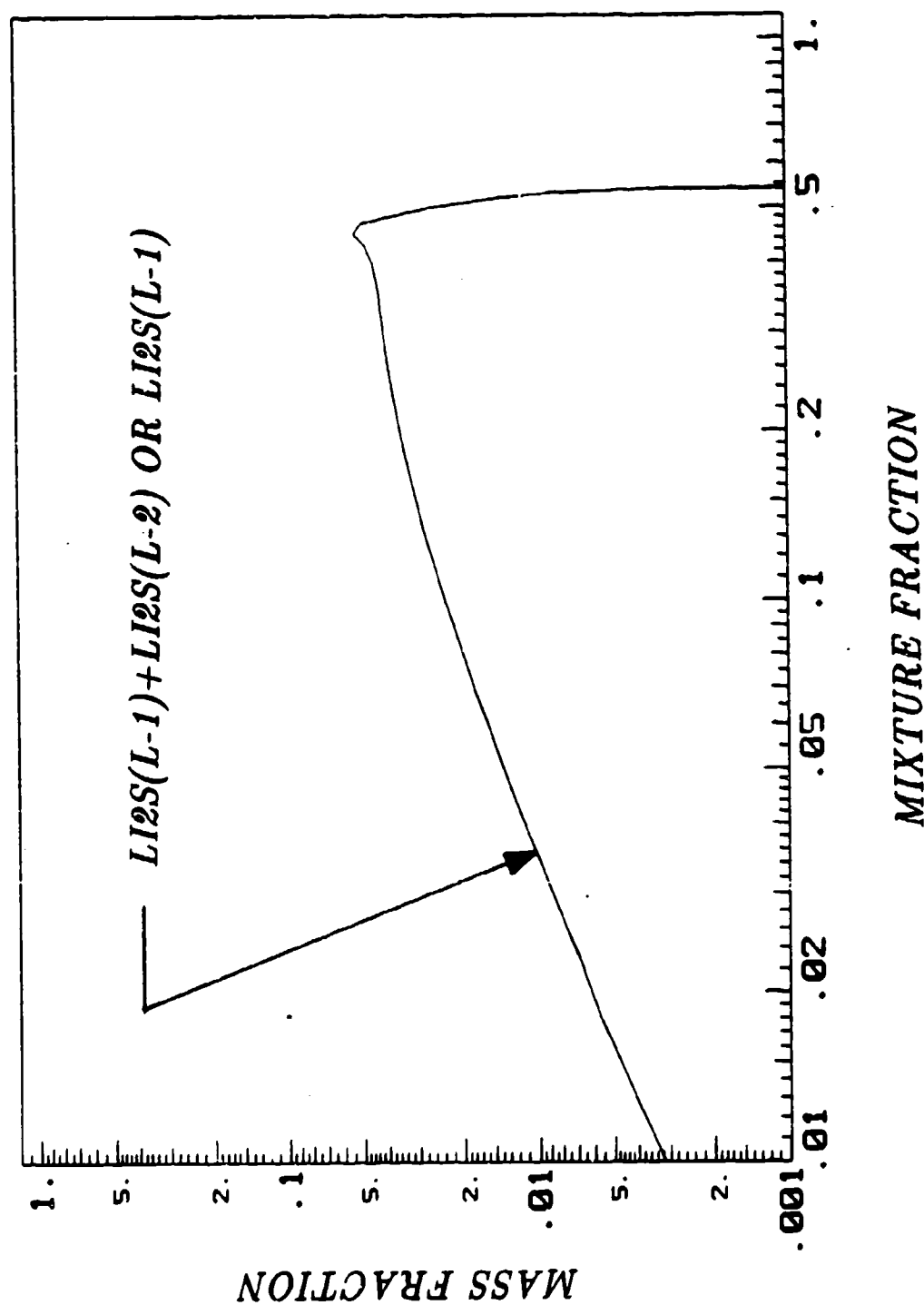


Fig.34 Equilibrium Compositions of $Li - SF_6$ System with Li at 1586 K and SF_6 Gas at 298 K

VARIATION OF MEAN QUANTITIES ALONG THE CENTER LINE

$T_{\infty} = 1130 \text{ K}$ (6A)

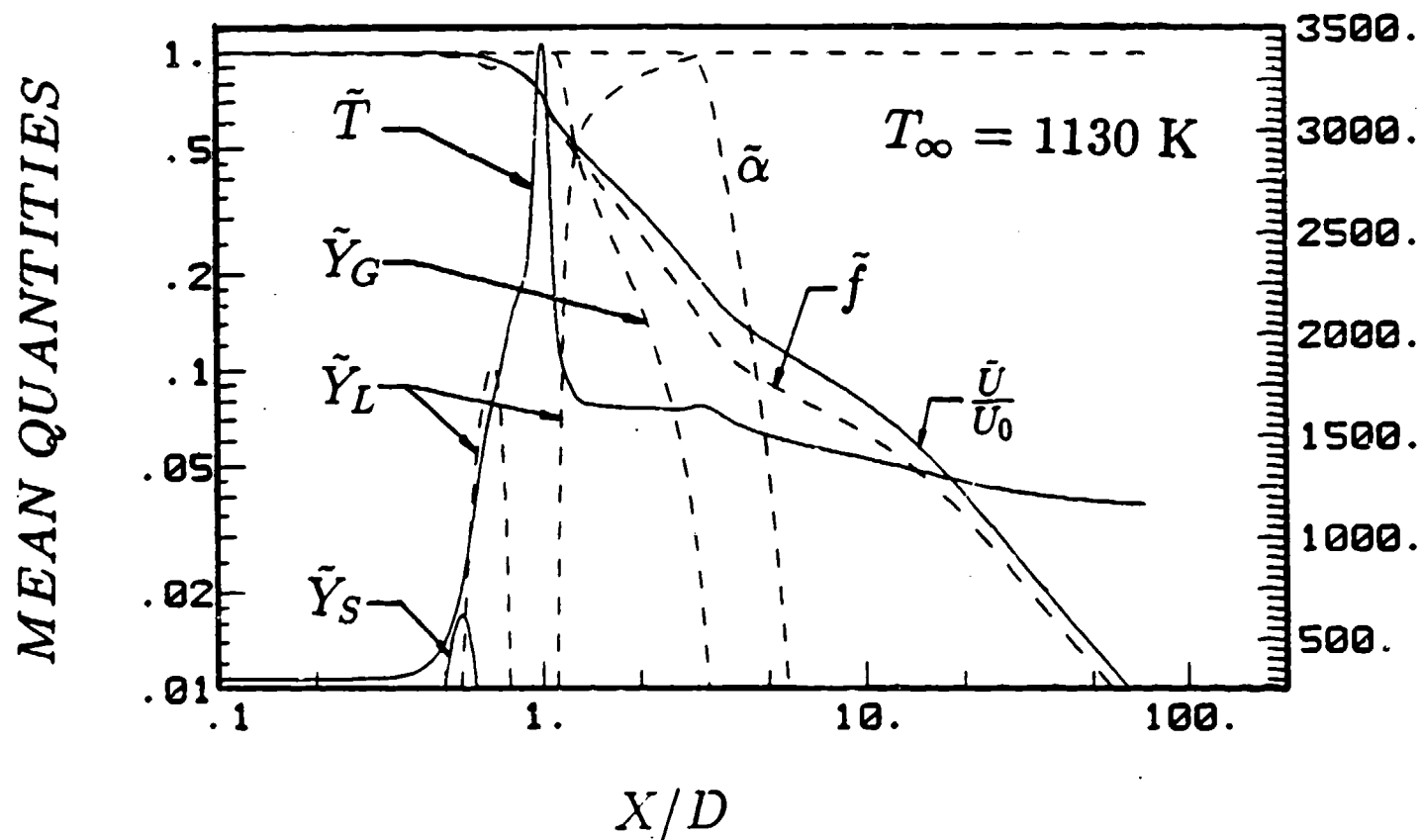


Fig.35 Predicted Mean Quantities Along The Jet Axis

SF_6 Gas (298K) Discharged In Molten Li (1130K)

VARIATION OF MEAN QUANTITIES ALONG THE CENTER LINE

$T_{INF} = 1358\text{K}$ (6A)

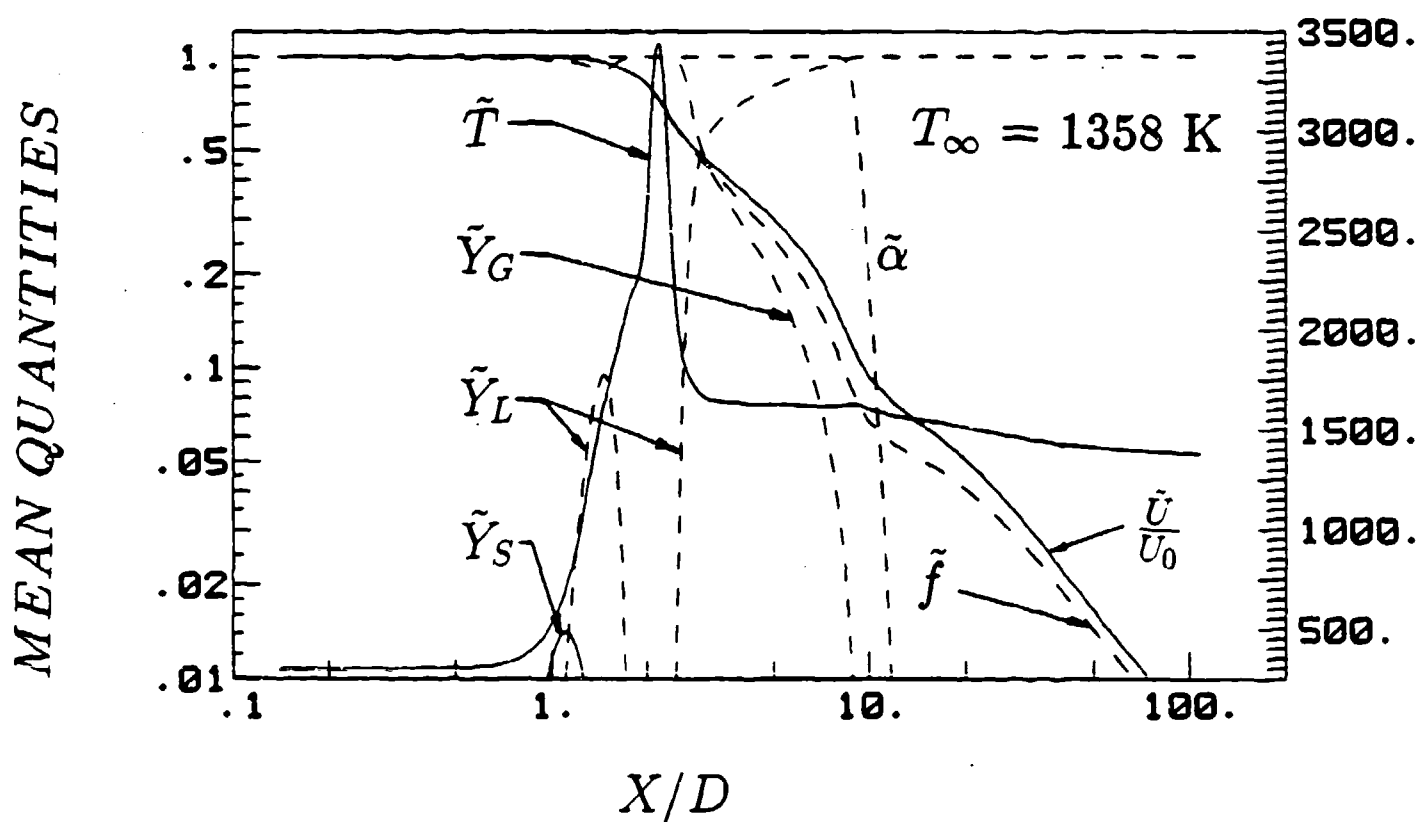


Fig.36 Predicted Mean Quantities Along The Jet Axis

SF_6 Gas (298K) Discharged In Molten Li (1358K)

VARIATION OF MEAN QUANTITIES ALONG THE CENTER LINE

TINF=1415K (GA)

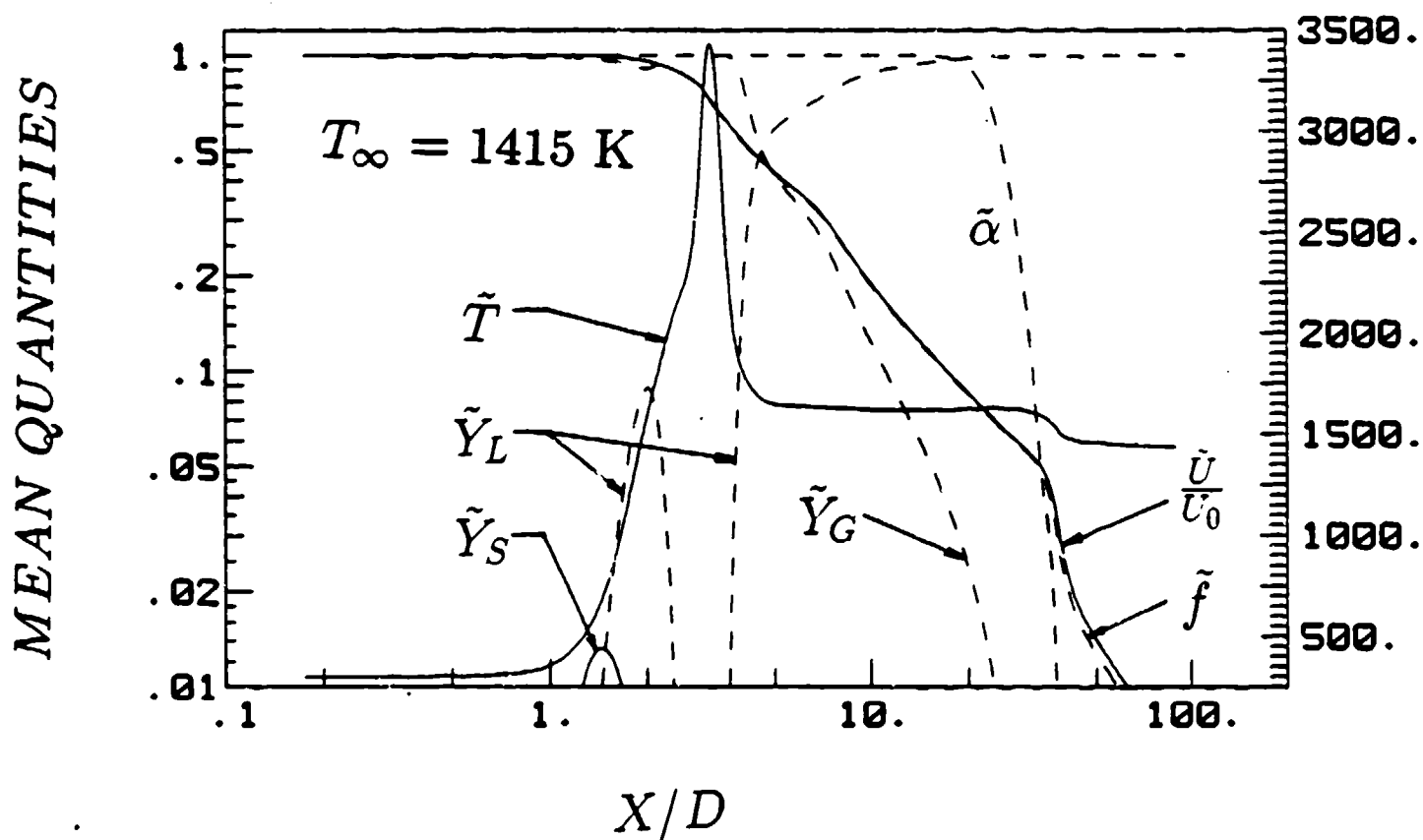


Fig.37 Predicted Mean Quantities Along The Jet Axis

SF_6 Gas (298K) Discharged In Molten Li (1415K)

VARIAION OF MEAN QUANTITIES ALONG THE CENTER LINE

TINF=1586K (GA)

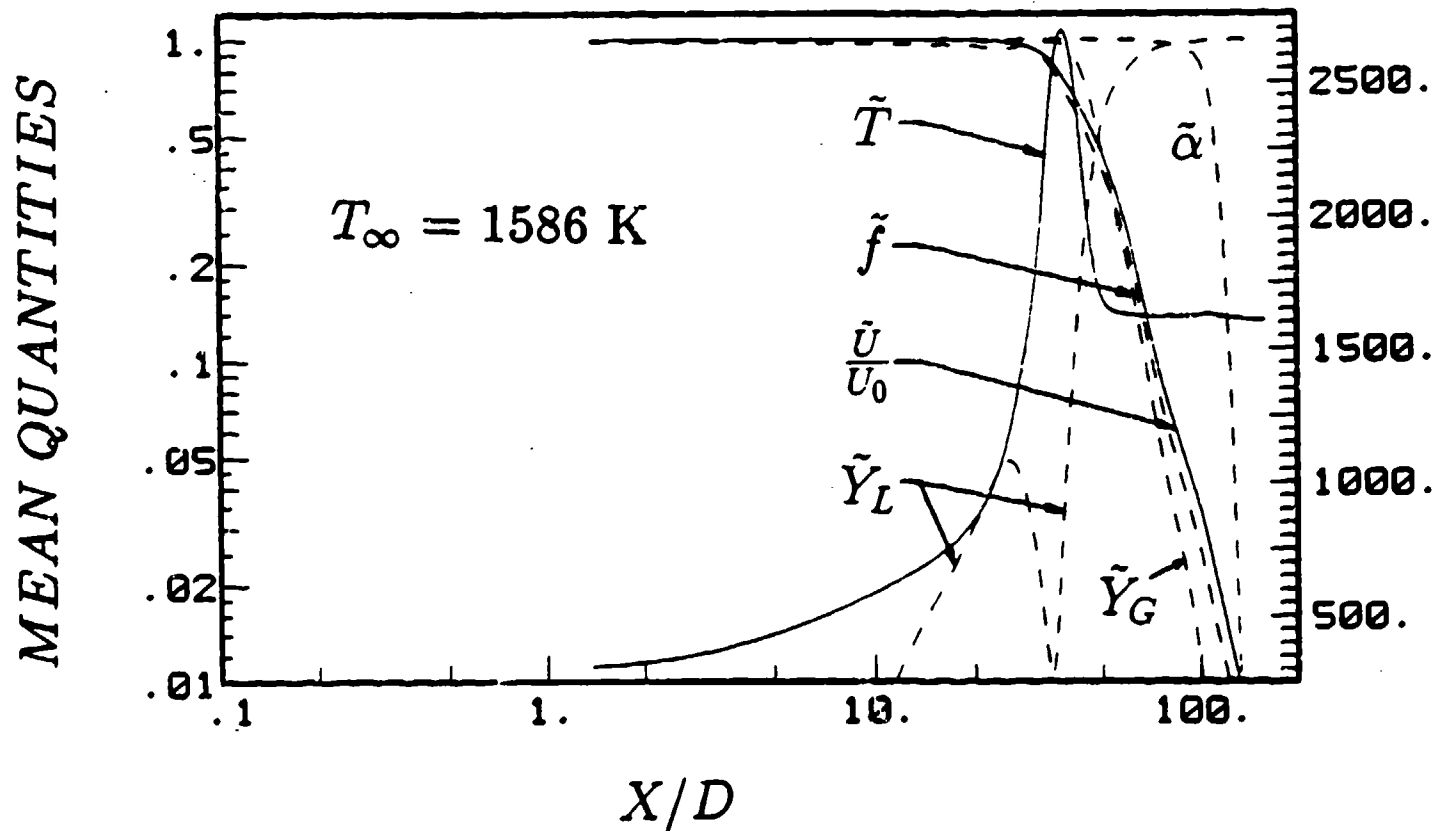


Fig.38 Predicted Mean Quantities Along The Jet Axis

SF_6 Gas (298K) Discharged In Molten Li (1586K)

APPENDIX A. Equilibrium Computer Program And Results For $Li - SF_6$ Reaction

APPENDIX B. Flow Structure Computer Program And Results For $Li - SF_6$ Reaction

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